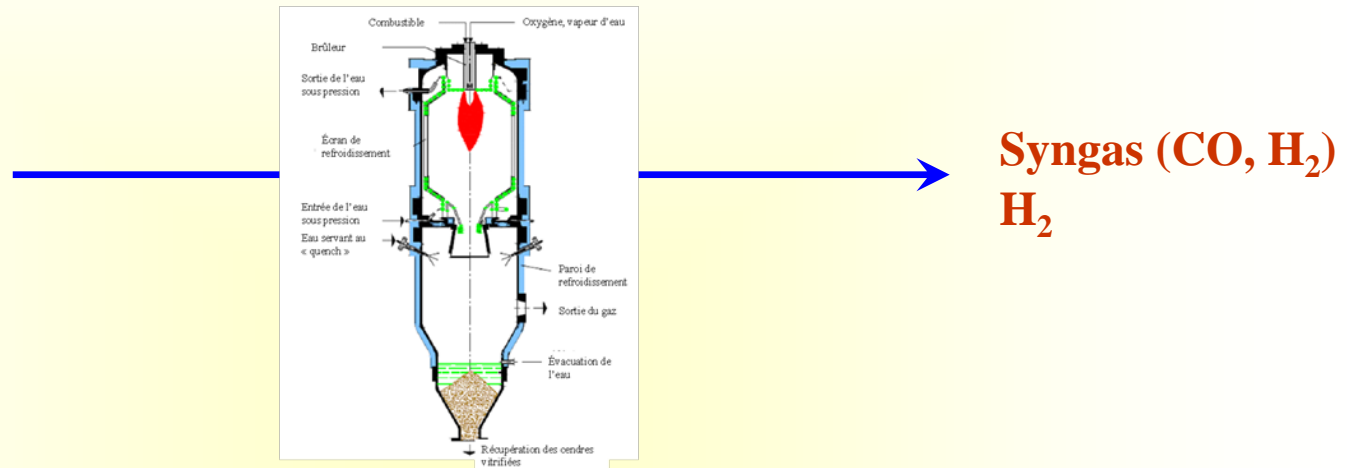


**Torrefaction of biomass:  
influence of operating conditions on products**

Jean-Michel **COMMANDRE**

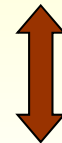
P. ROUSSET, G. LESUEUR, A. LEBOEUF, L. CHAFCHAOUNI

## Thermo-chemical conversion of biomass in entrained flow reactor (EFR)



**Syngas (CO, H<sub>2</sub>)  
H<sub>2</sub>**

- EFR {
- High temperature (1400°C) → -High quality syngas
  - Small amounts of residual hydrocarbons and solid carbon
  - Short residence time (≈ s) → Biomass **must be ground finely** (≈ 100μm) before injection



**Grinding consumes large amounts of energy**

**Torrefaction:** biomass pretreatment used to **reduce mechanical properties**

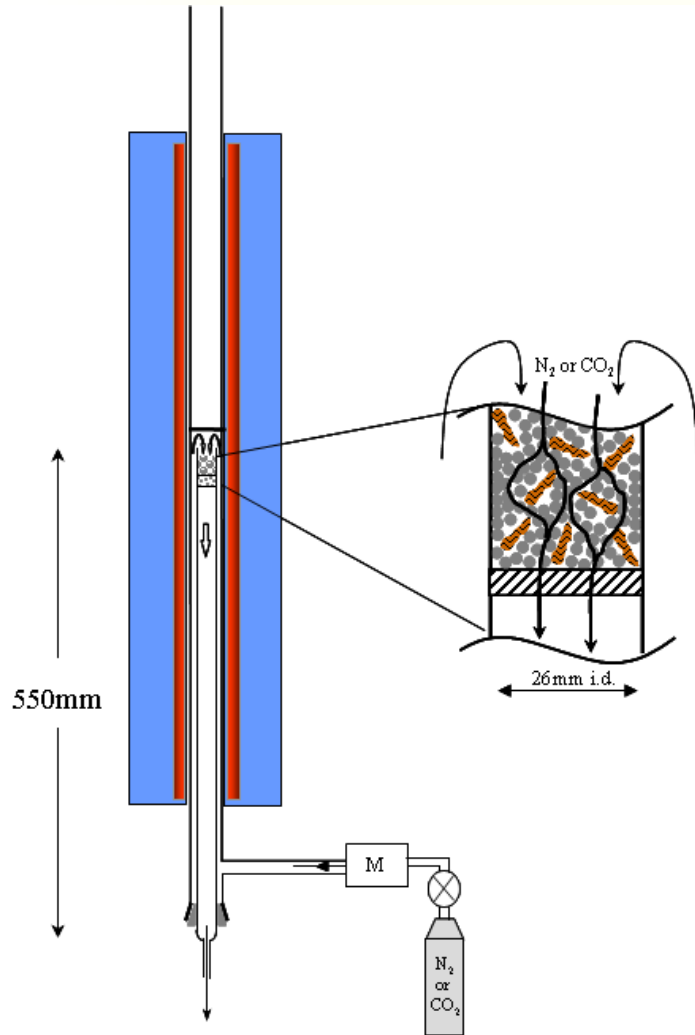
## Objectives:

Characterisation of **biomass torrefaction products**,

from **biomass** analysis to precise **mass balances**,

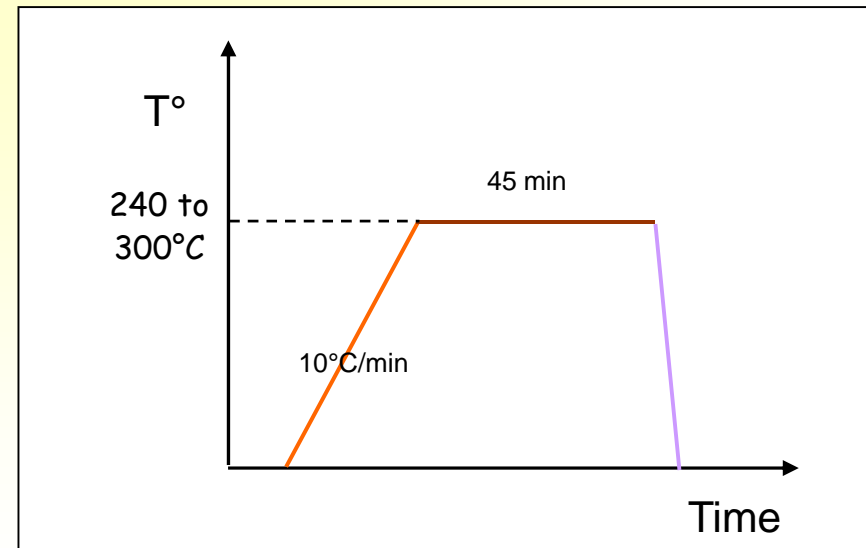
by the way of a complete quantification of the **products** released

# Torrefaction at laboratory scale: Crossed fixed bed reactor

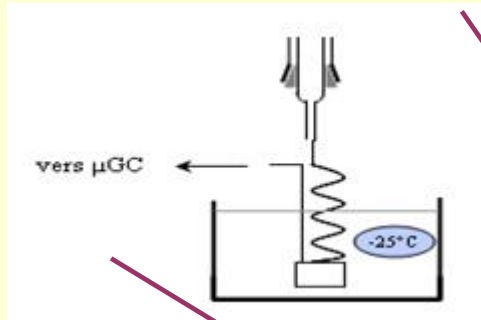
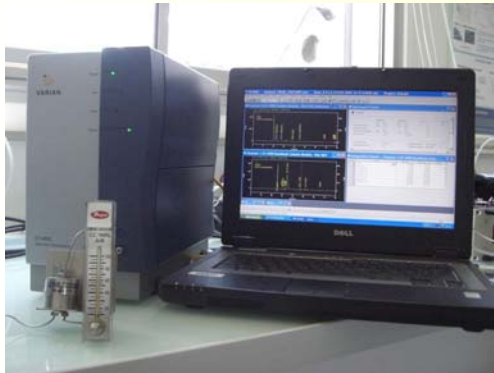


- control of gas and wood temperature
- control of gas nature and flow rate
- gas flow rate sufficiently high to avoid heterogeneous reactions
- wood particles mixed with glass balls to ensure:
  - good contact between gas and wood particles
  - homogeneous gas flow inside the bed

## Operating conditions



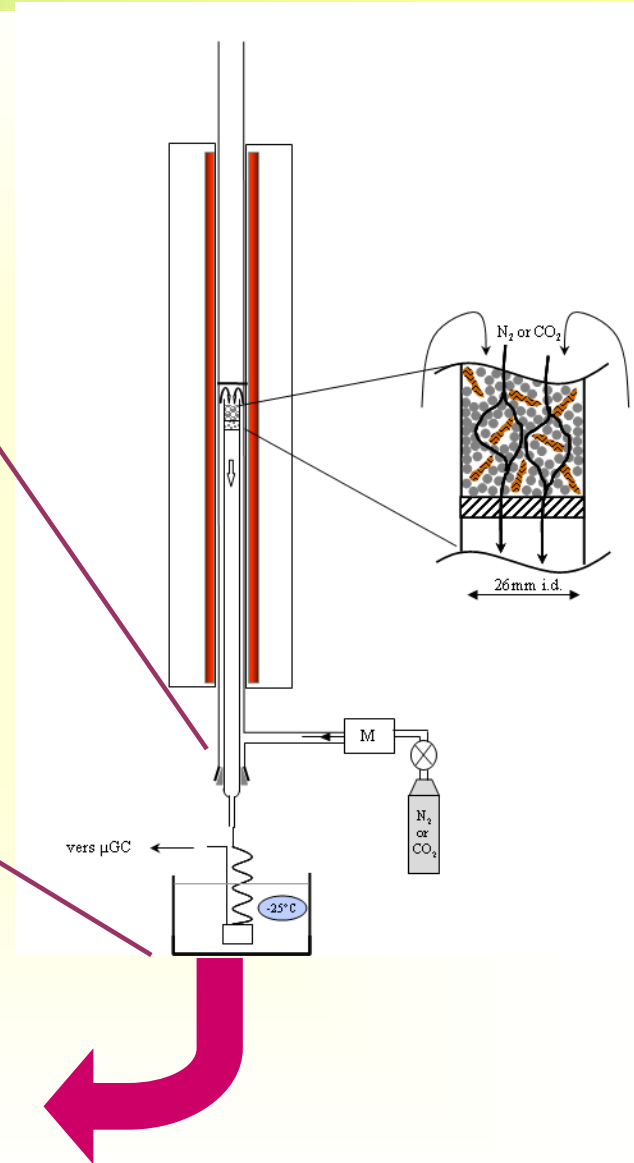
$\mu$ GC



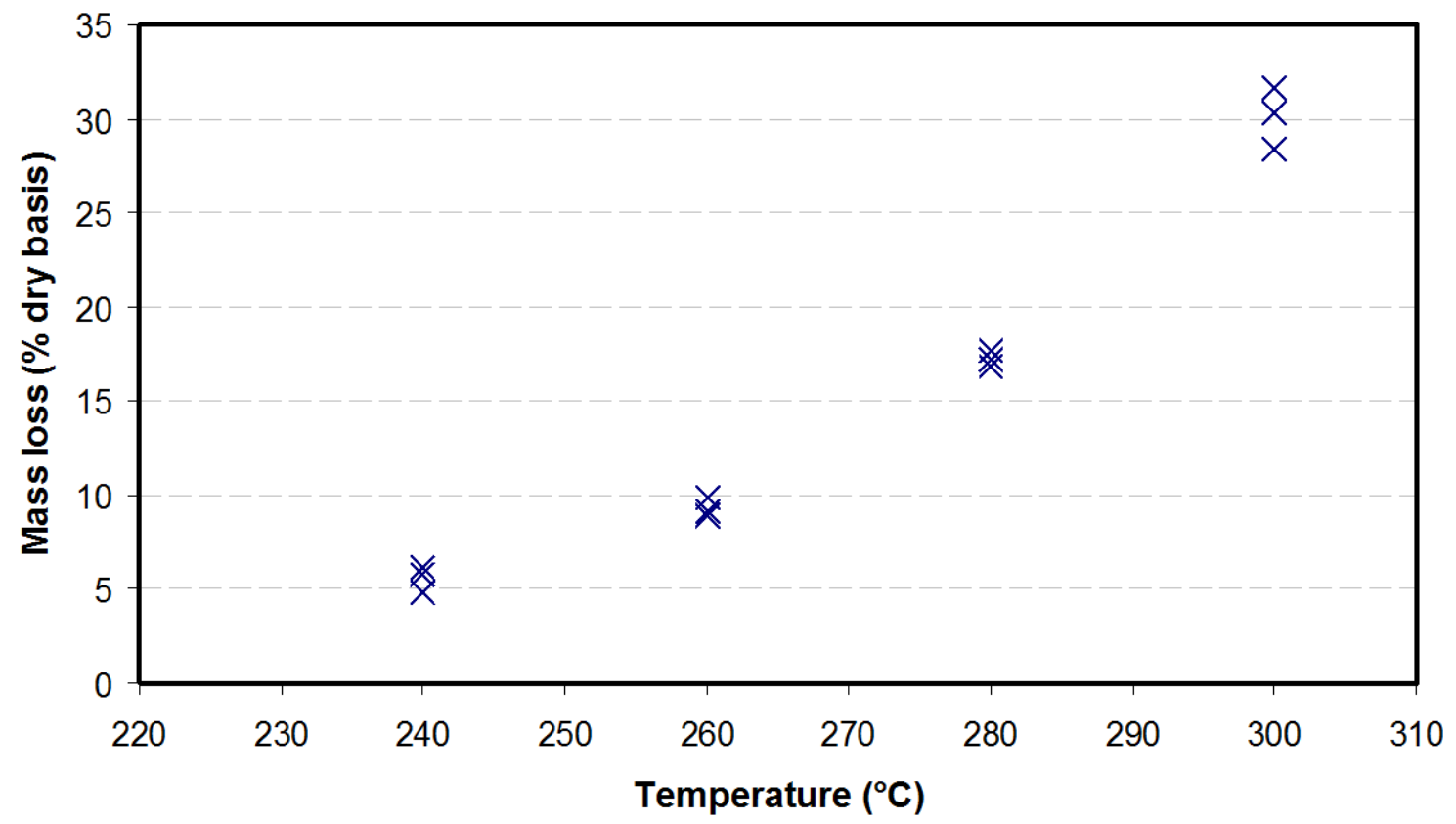
Karl-Fischer



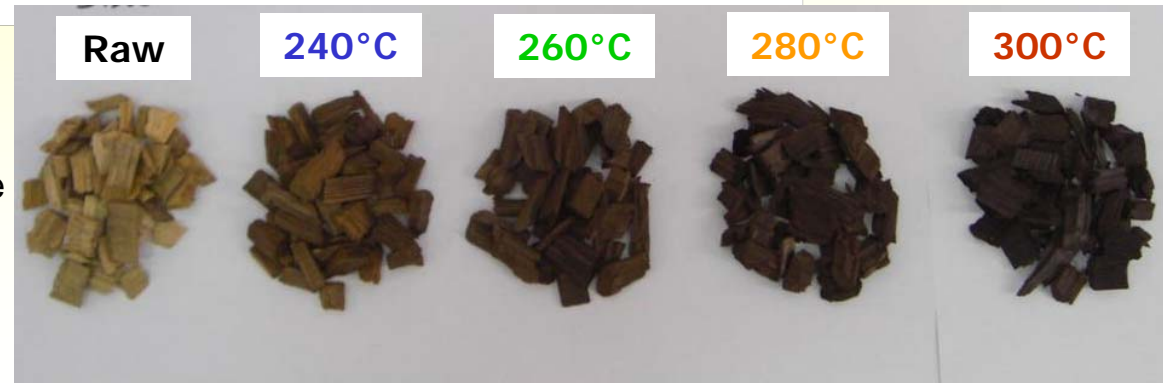
GC-MS

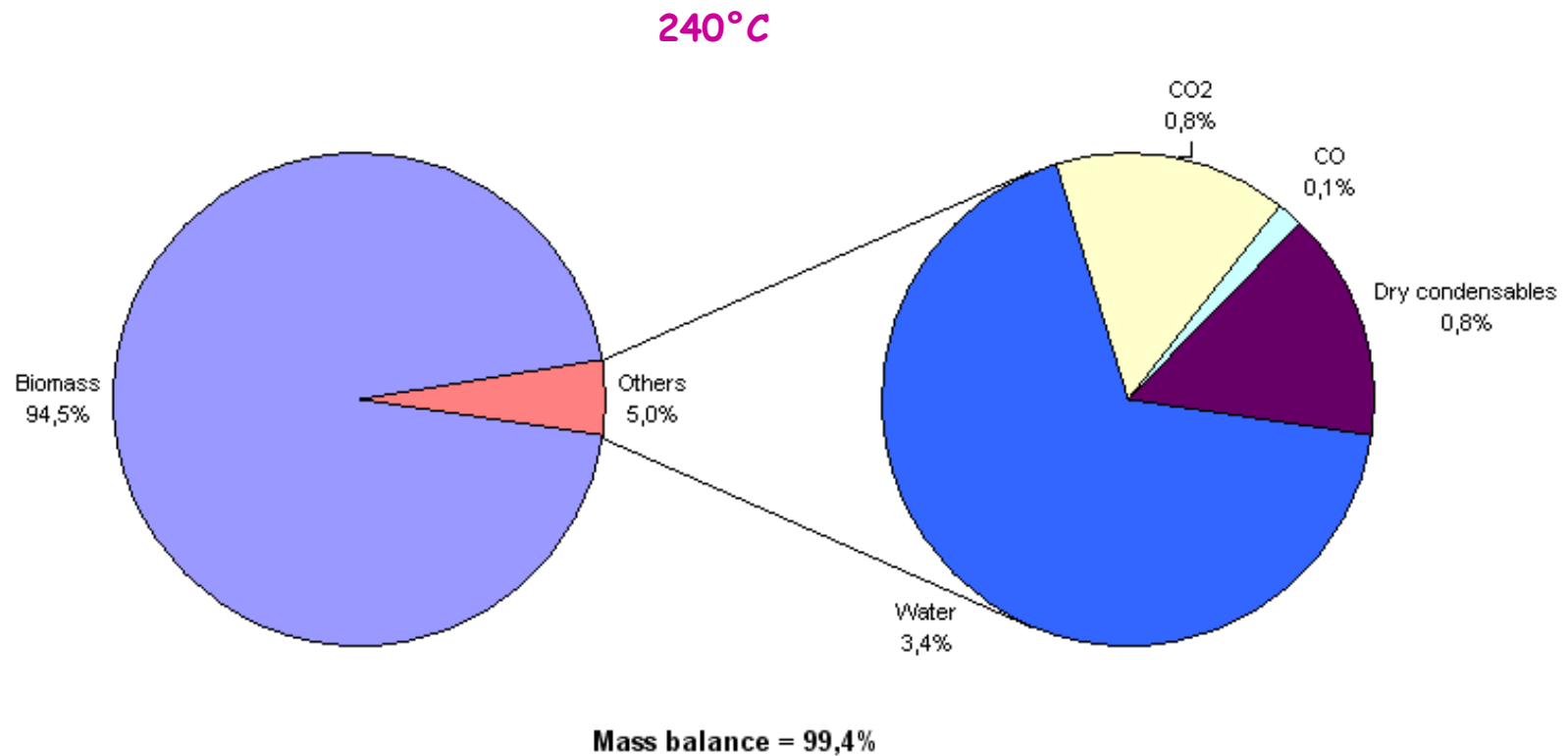


Pine wood

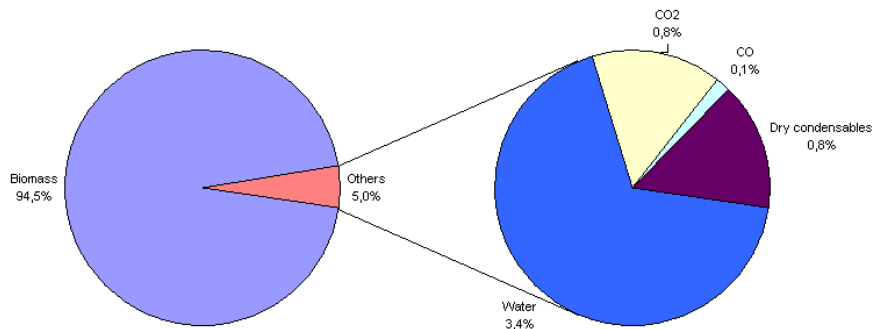


- Good reproducibility
- Increase of mass loss with temperature



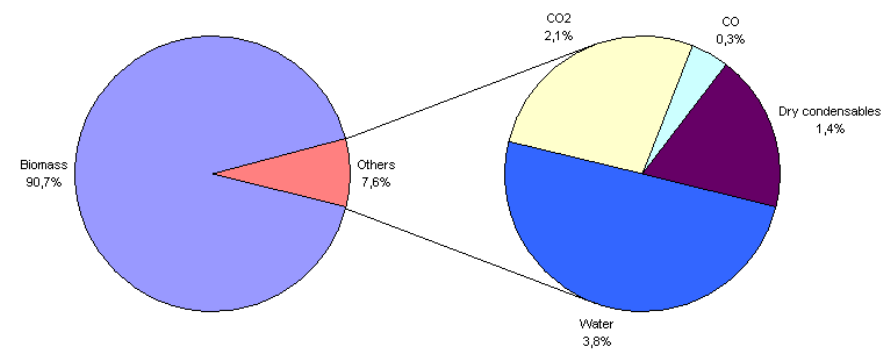


240°C



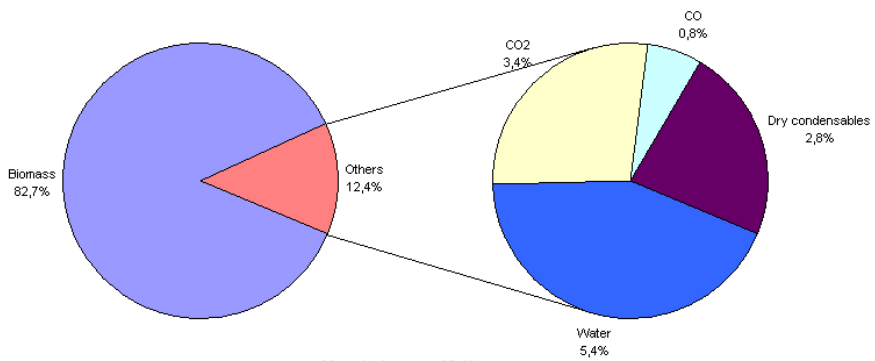
Mass balance = 99,4%

260°C



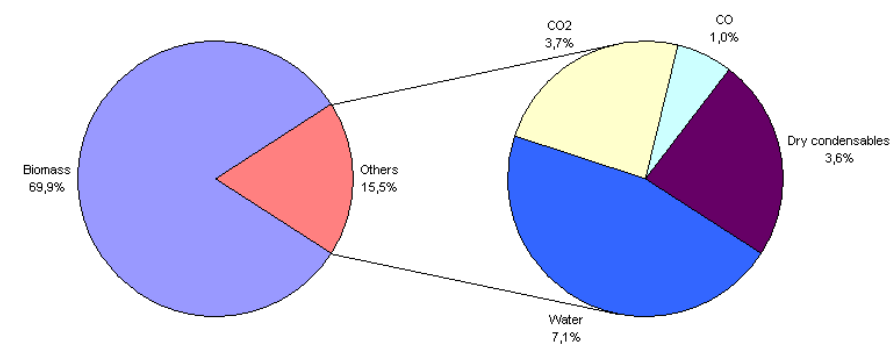
Mass balance = 98,3%

280°C



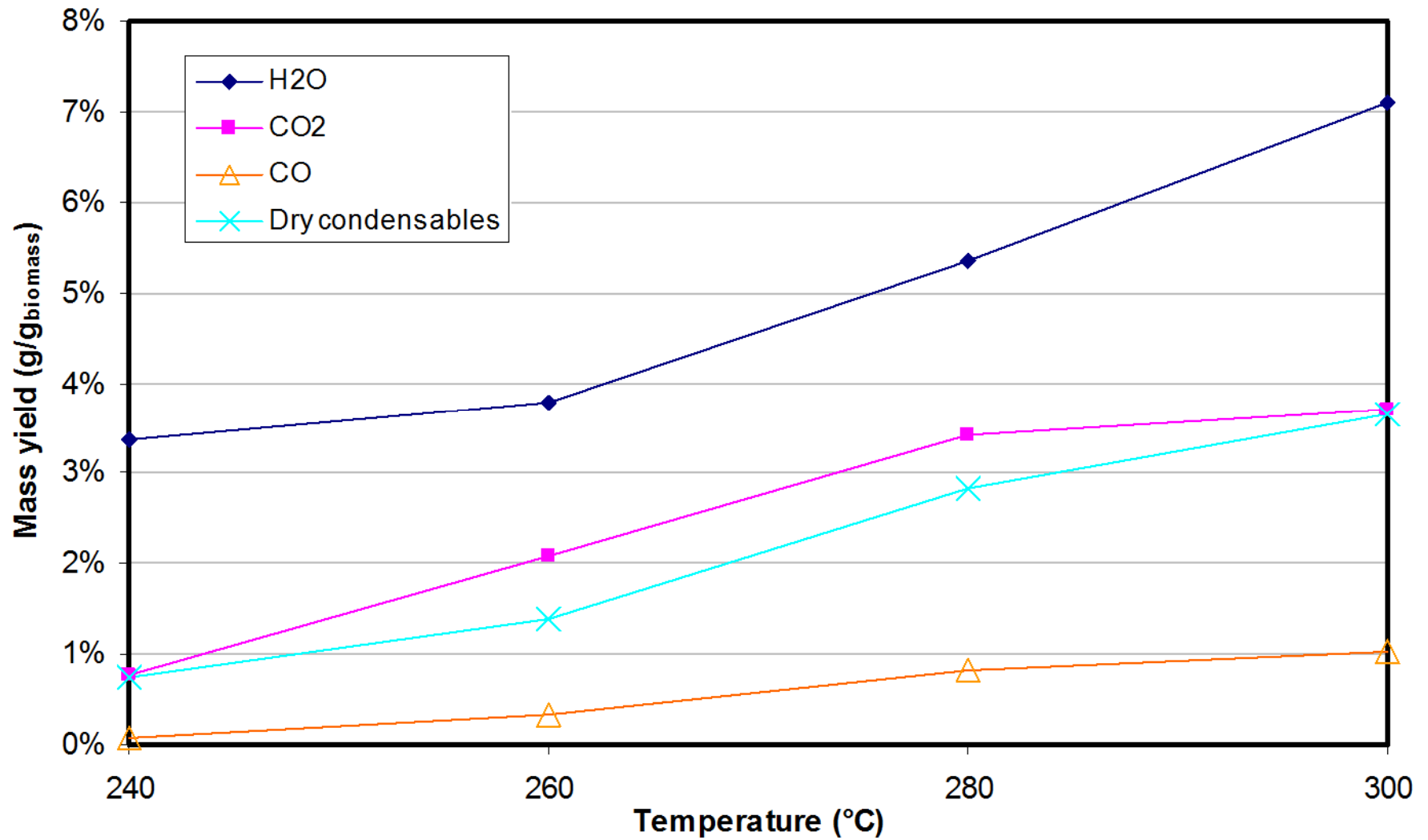
Mass balance = 95,1%

300°C

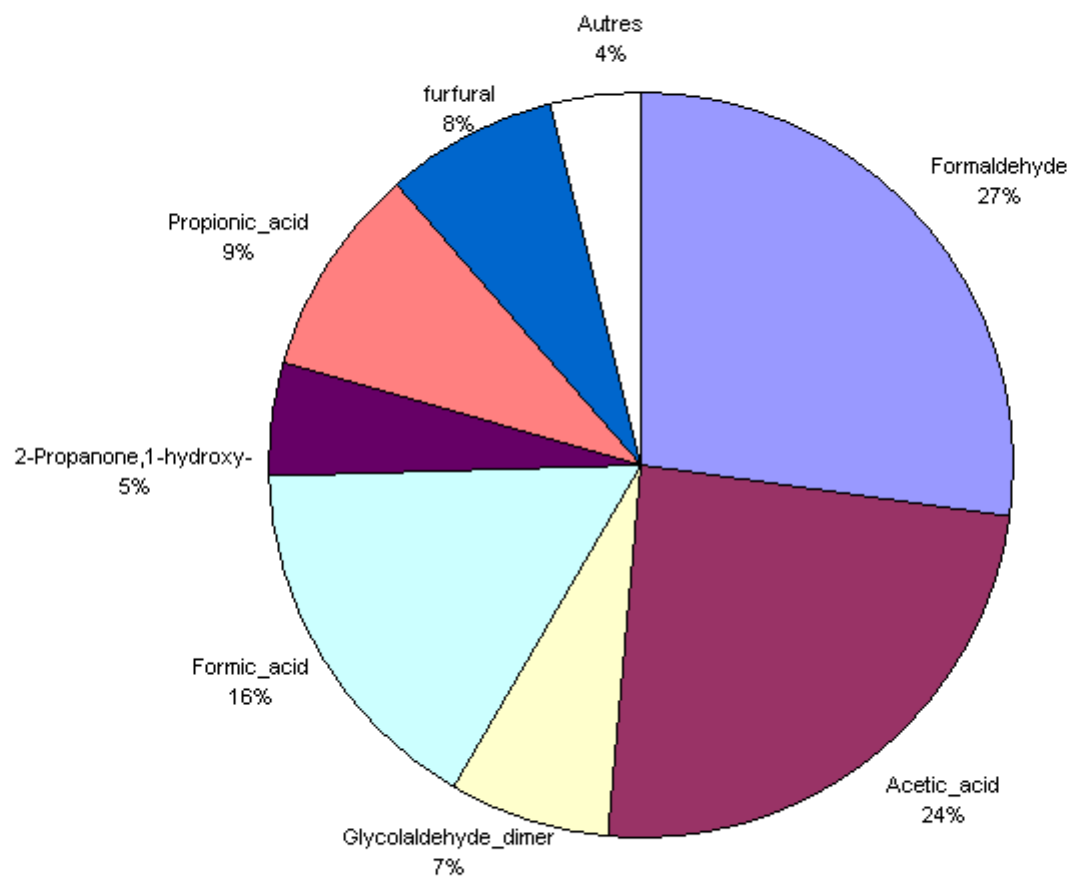


Mass balance = 85,4%

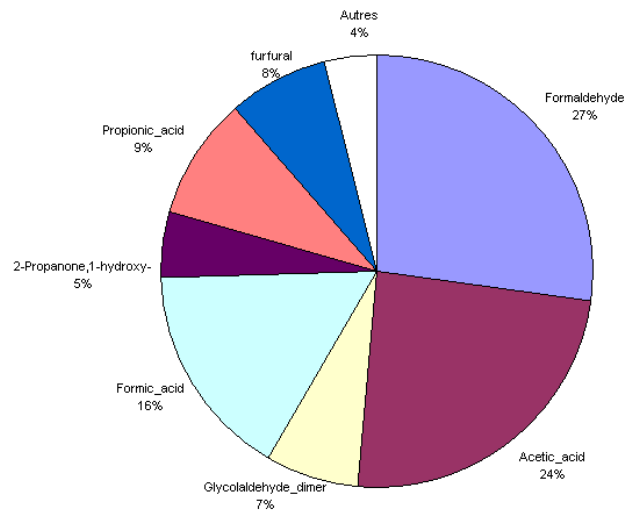




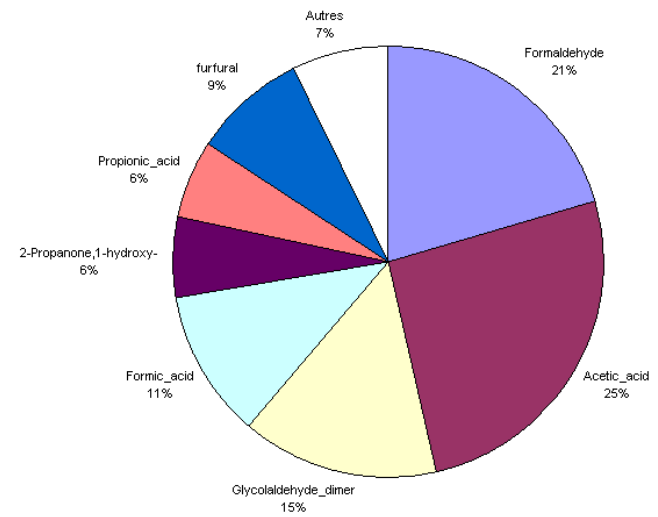
240°C



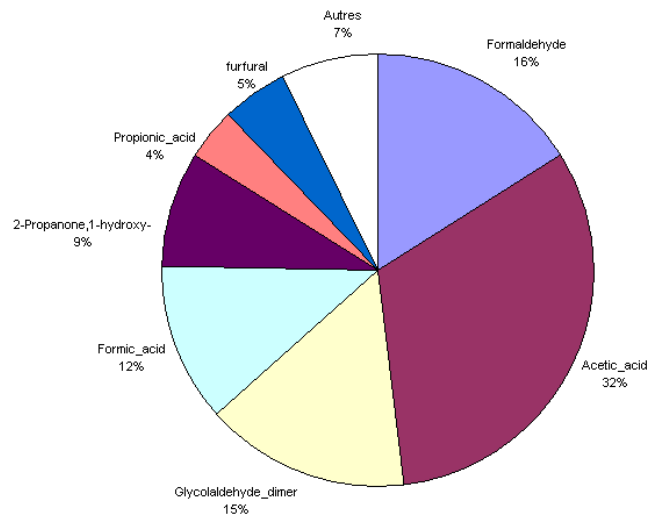
240°C



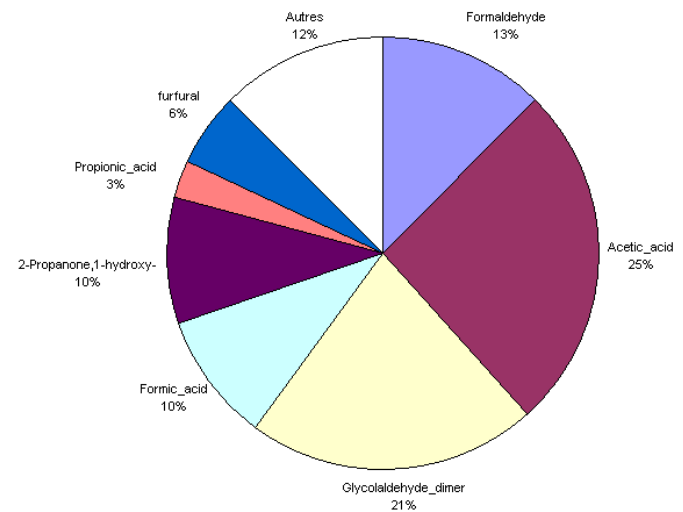
260°C

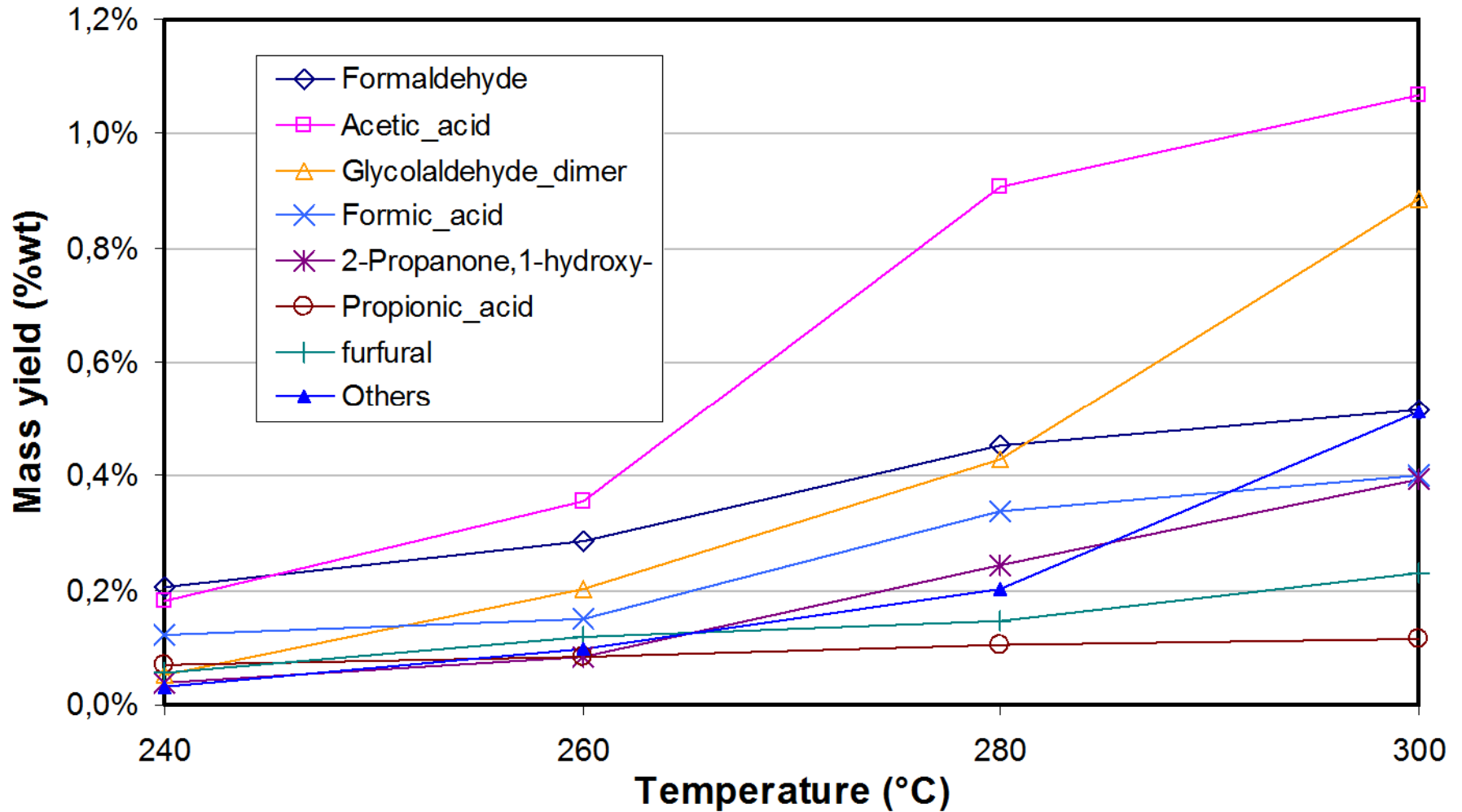


280°C

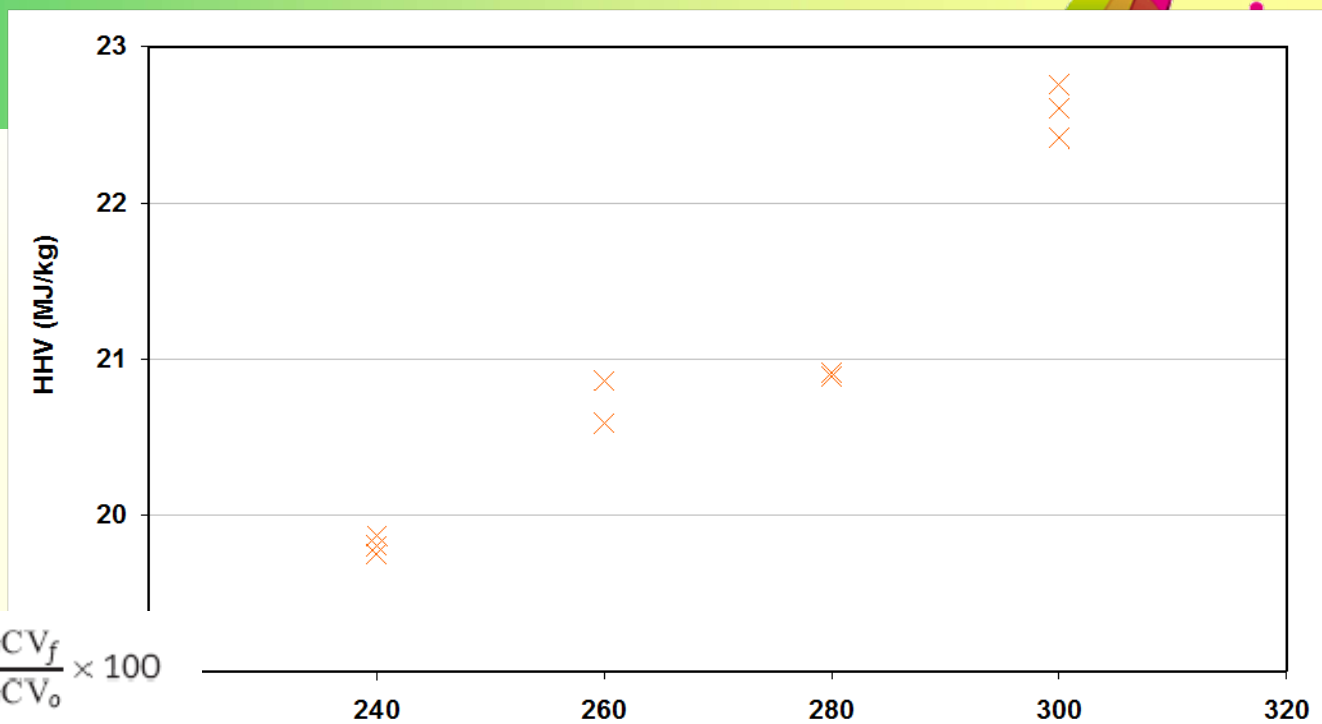


300°C



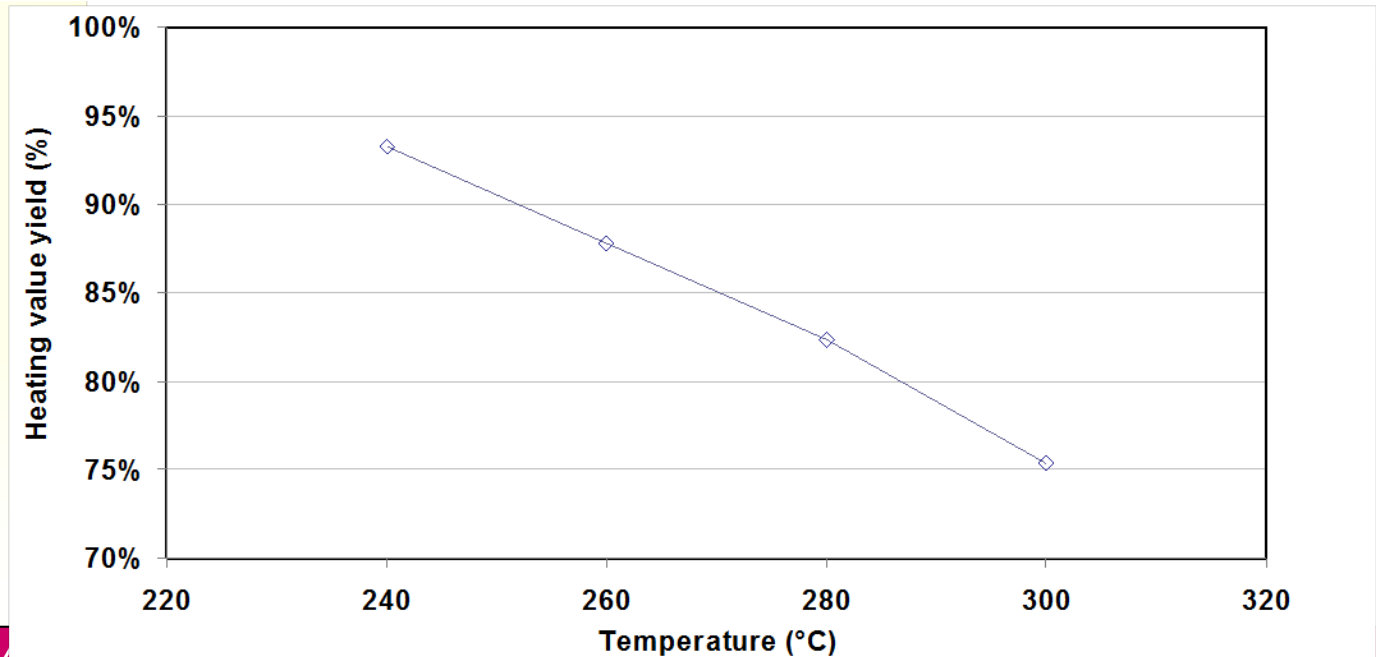


# Heating value

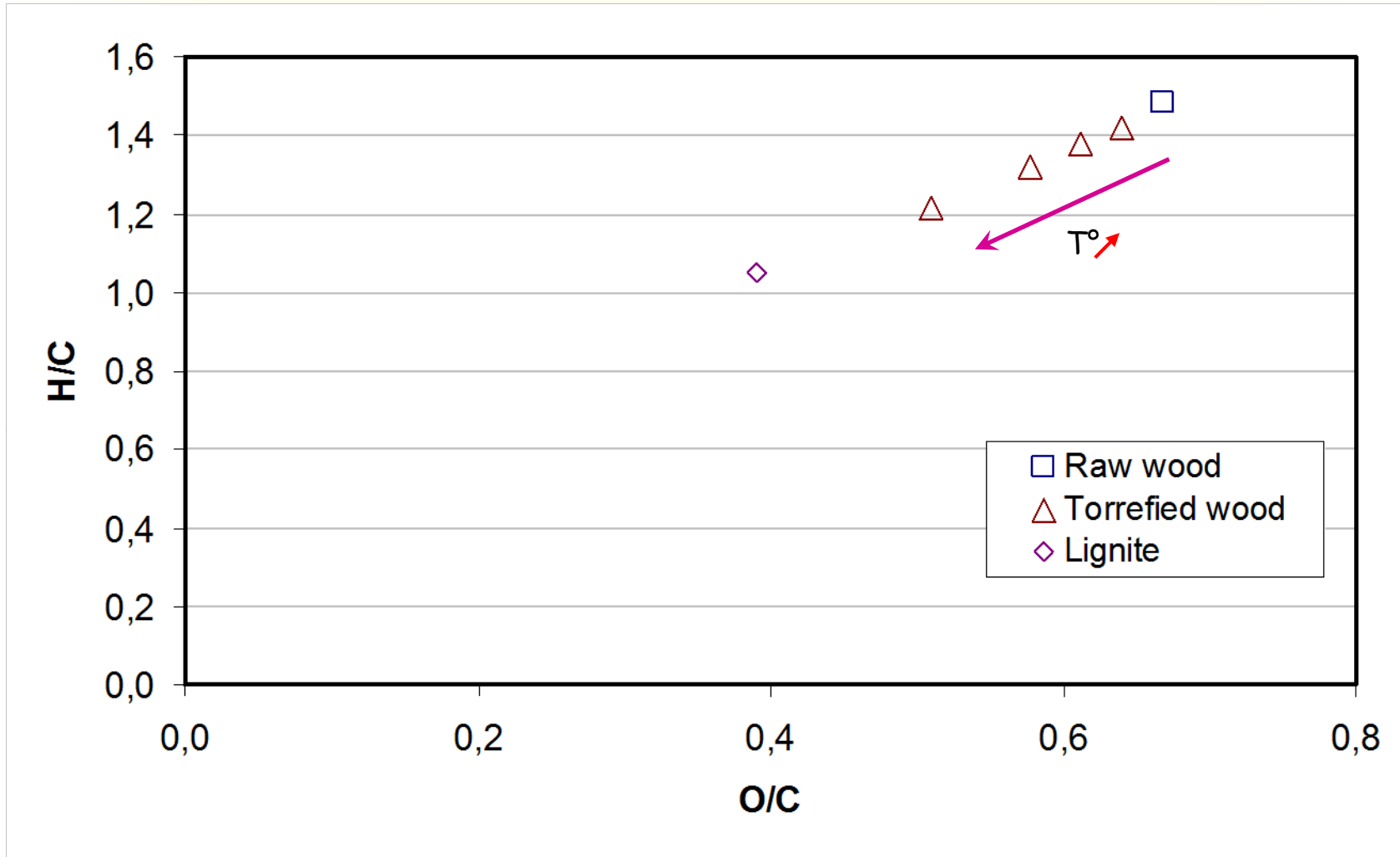


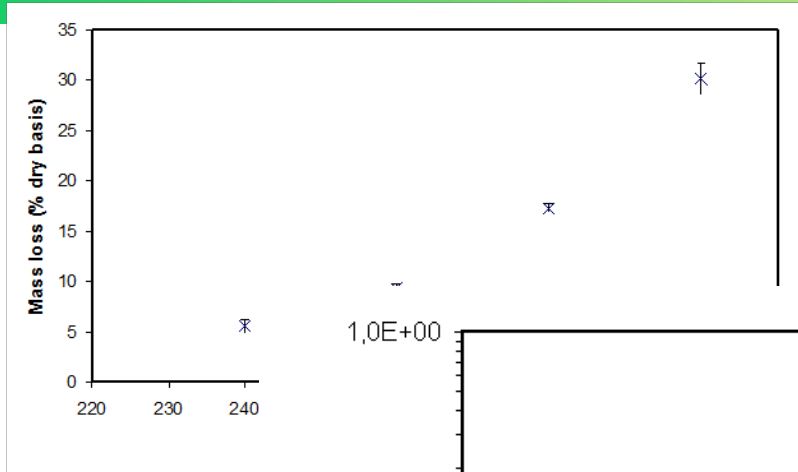
$$\text{Heating value yield}(\%) = \frac{M_f \text{ GCV}_f}{M_o \text{ GCV}_o} \times 100$$

(Arias, 2008)



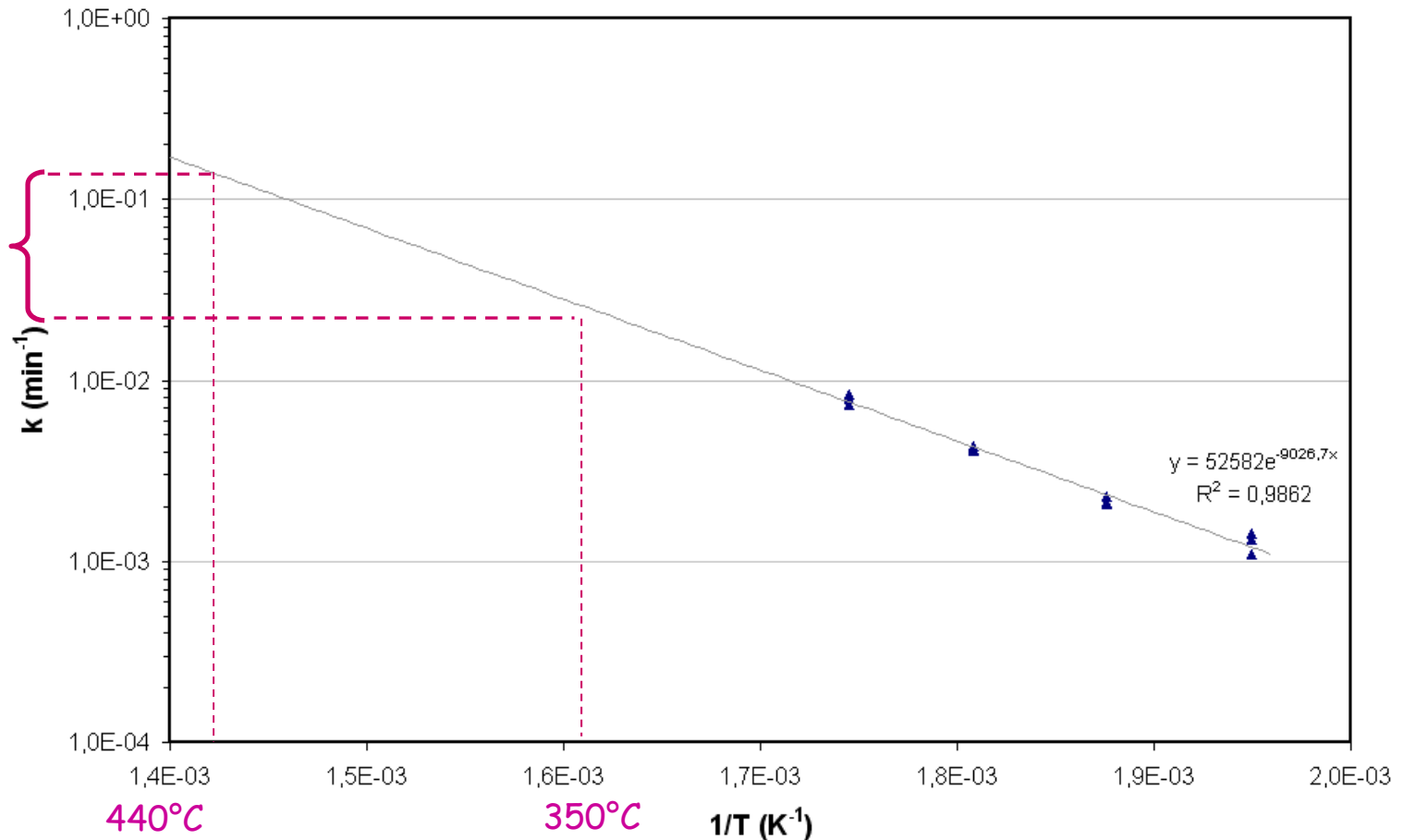
Van Krevelen diagram





## Simple first-order kinetic model

$$\frac{dm}{dt} = -k \cdot m$$



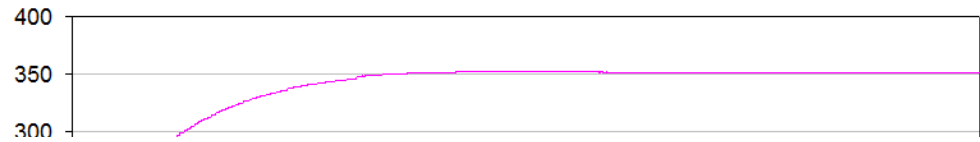
Mass loss  $\approx$  20%  
Resid. time  $\approx$  min

# Torrefaction at high heating rate

## Operating conditions:

Temperature = **350°C**

Residence time: **5 min**

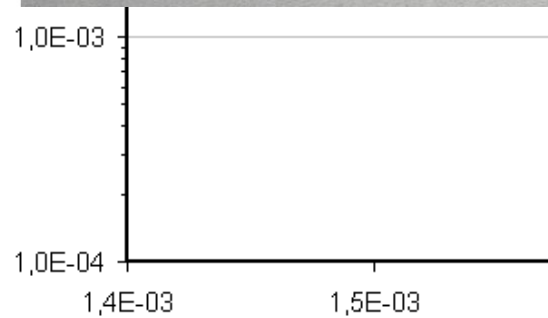


1,0E+00

### Raw biomass



### Torrefied biomass

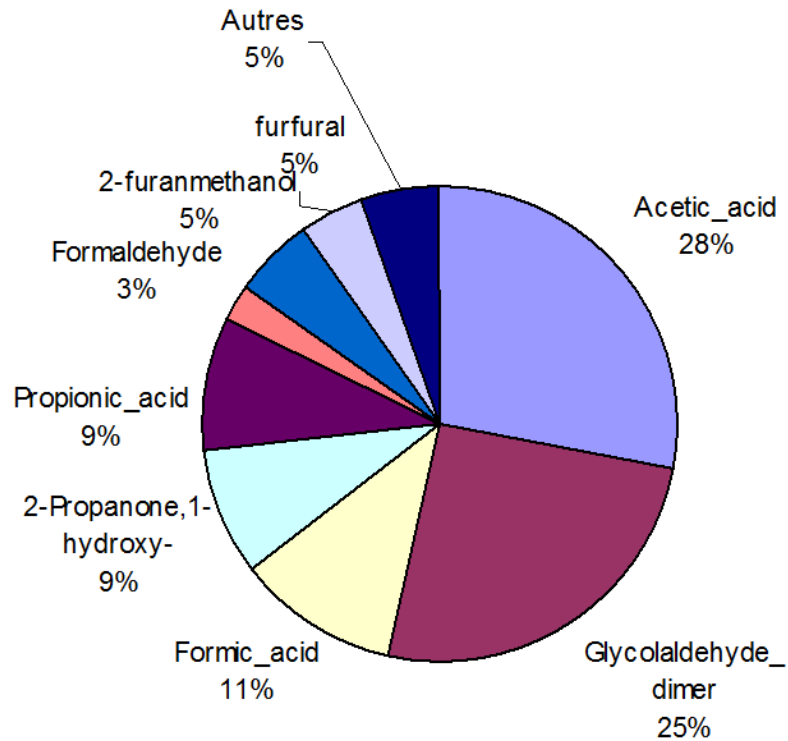


### « Crushed » Torrefied biomass





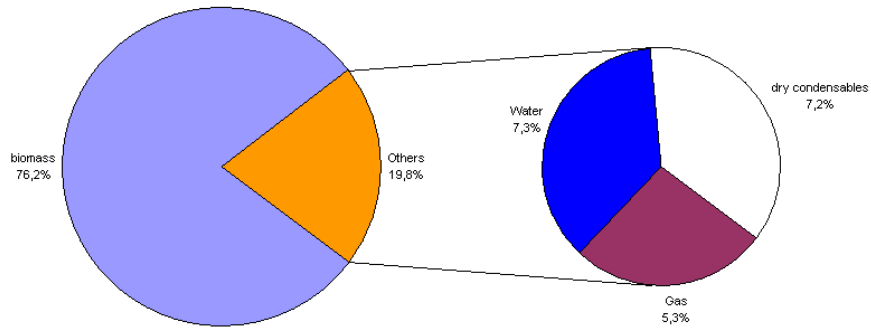
## Detailed mass balance



Compared to 280 and 300°C:

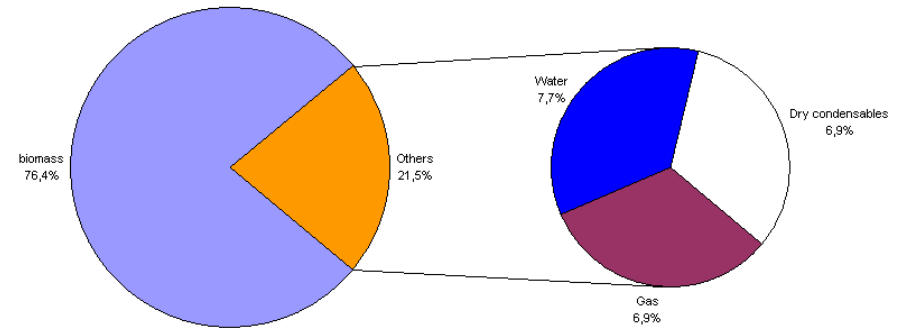
- Less formaldehyde
- Much more propionic acid
- Slightly similar acetic acid and glycolaldehyde contents

### Triticale

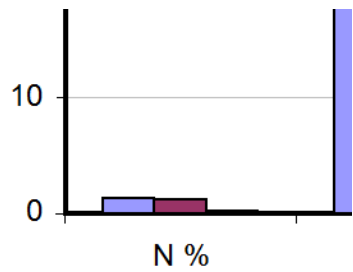


Mass balance = 95,9%

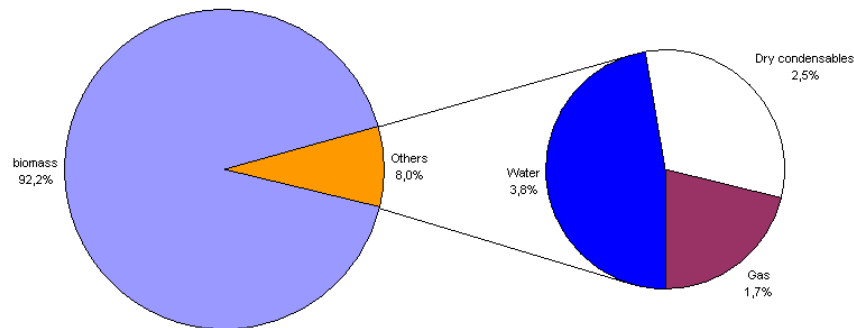
### Fescue



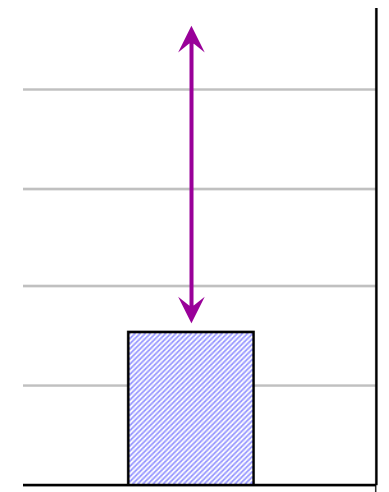
Mass balance = 97,9%



### Pine



Mass balance = 100,2%



- **A complete characterisation of products of biomass torrefaction has been realised**
- **Volatile matters released mainly contain water, dry condensable species, CO<sub>2</sub> and CO**
- **Dry Condensable species mainly contain acids, aldehydes and ketones**
- **High heating rate influences significantly the torrefaction products**
- **Significant influence of the nature of biomass**
- **Work in progress:**
  - **Cellulose, Hemicellulose and Lignin contents**
  - **Grindability: energy consumption during grinding**