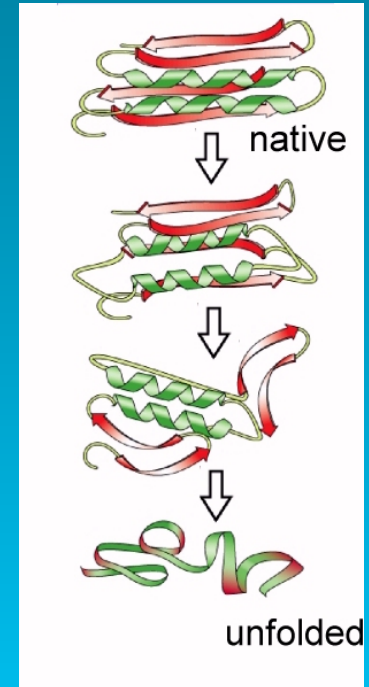
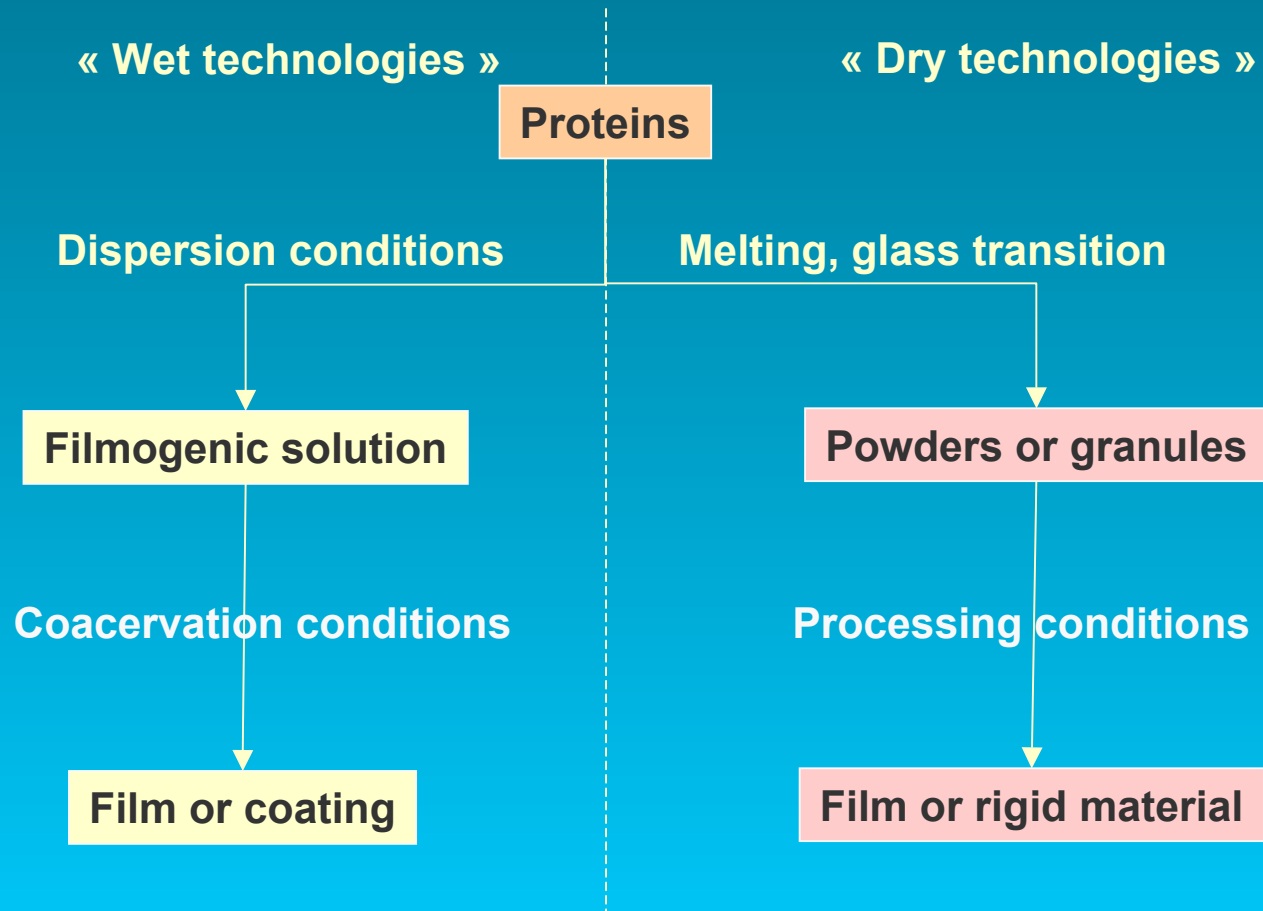


# Technical feasibility of common polymer technologies applied to natural polymers

- Casting: *Paulo Sobral, FZEA-USP Brazil*
- Spread Coating: *Patricia Eisenberg, Plasticos-INTI Argentina*
- Extrusion and thermomoulding : *Laurent Ferry, EMA, France*

# Introduction

## → Protein processing



# Raw matter

## ➔ Cottonseed cakes

### ➔ Complex materials

#### ■ Composition

○ proteins, lipids, cellulose, sugars...

#### ■ Different parts

○ Kernels, shells, linter

### ➔ Effect of oil extraction process

#### ■ Protein modification

## ➔ Delipidated glandless cottonseed flour





**CASTING**

# Production of films by casting

**Colloidal Solution Applied on a Support**

**Drying**

**Flexible Films**

# Film forming solution

**Basic formulation**

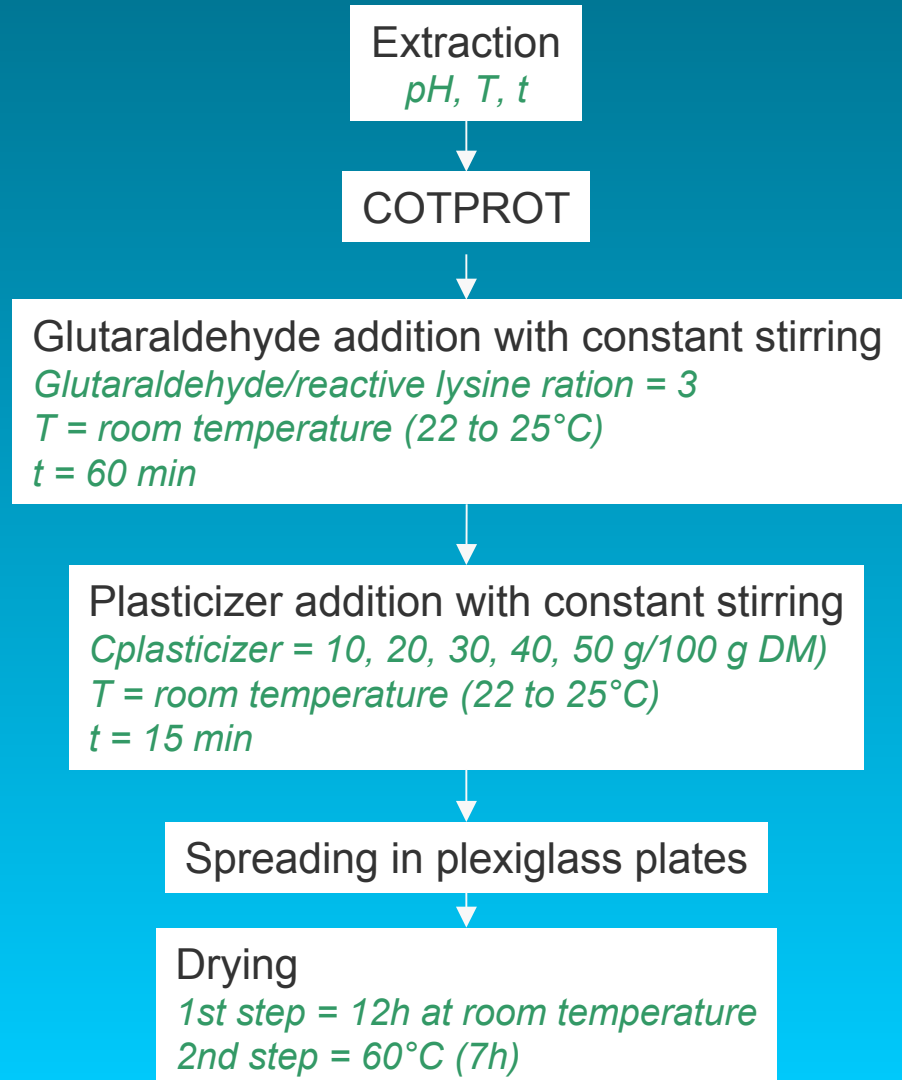
**COTPROT**

**pH agent**

**Plasticizer**

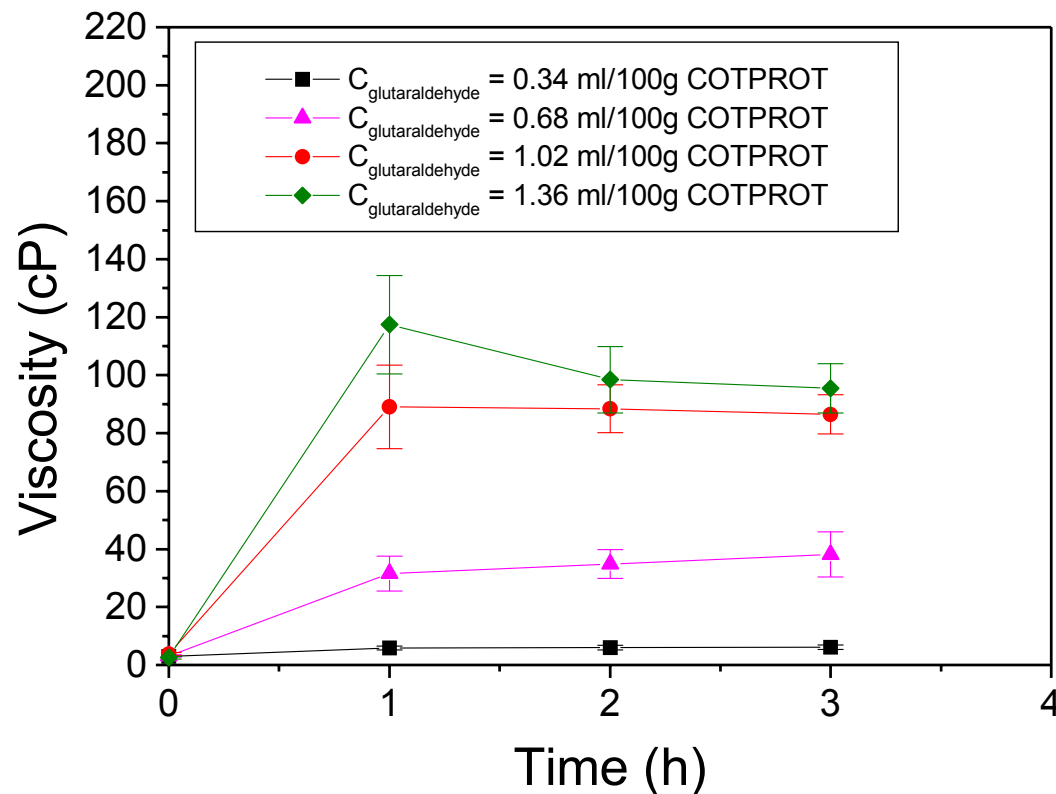
**Crosslinking agent**

# Film production steps

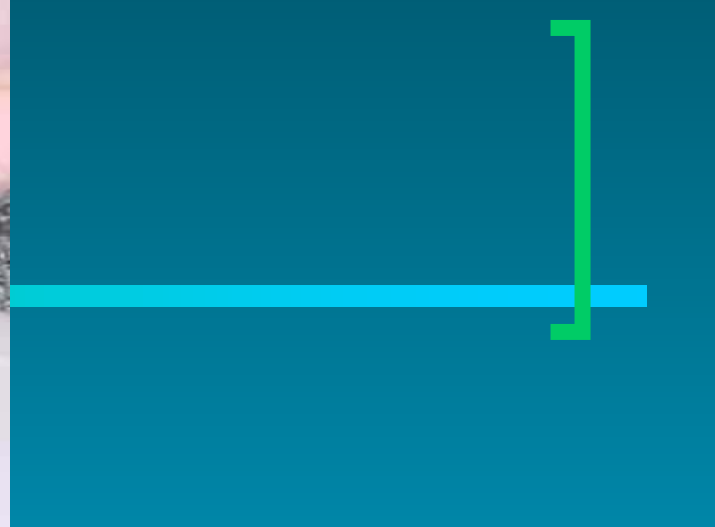


# Controlling the cast processing

## Viscosity of the solution

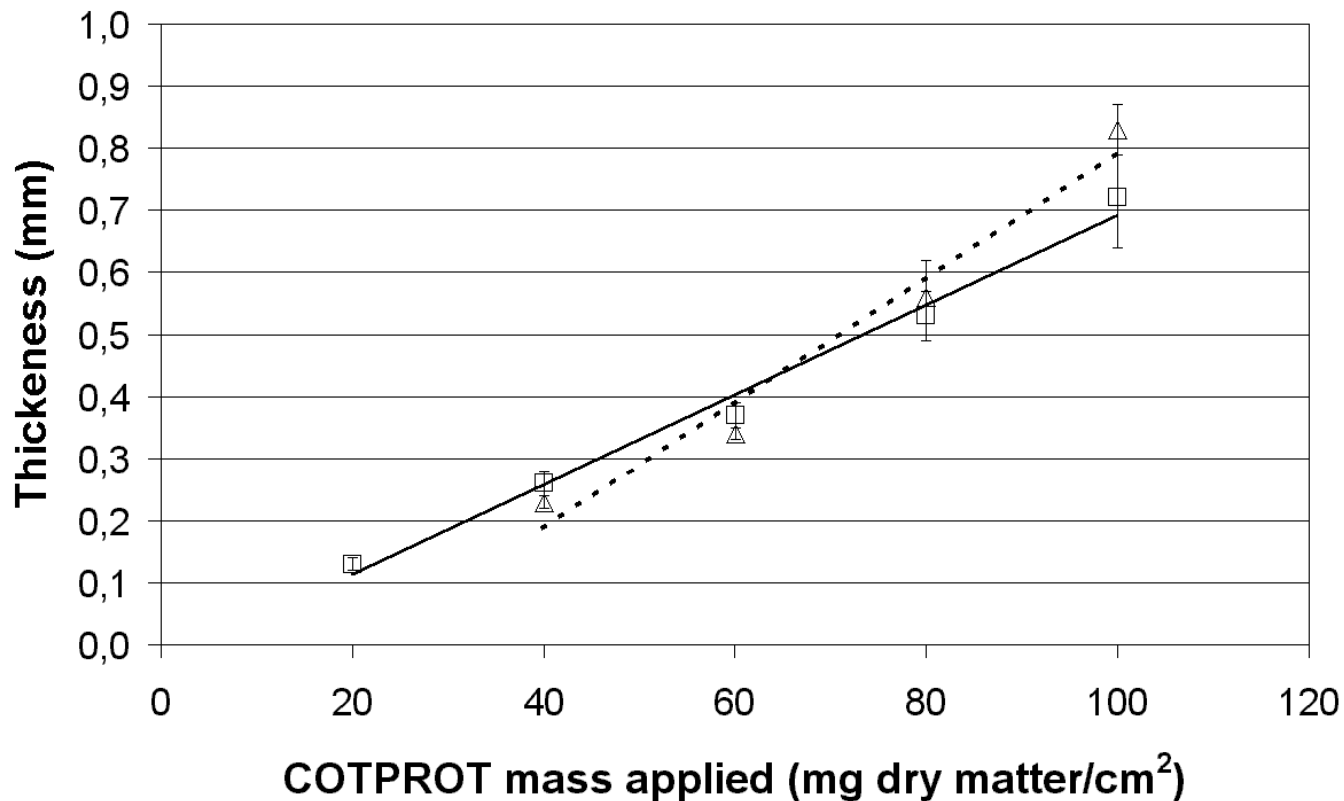






# Controlling the cast processing

## Control of thickness of films

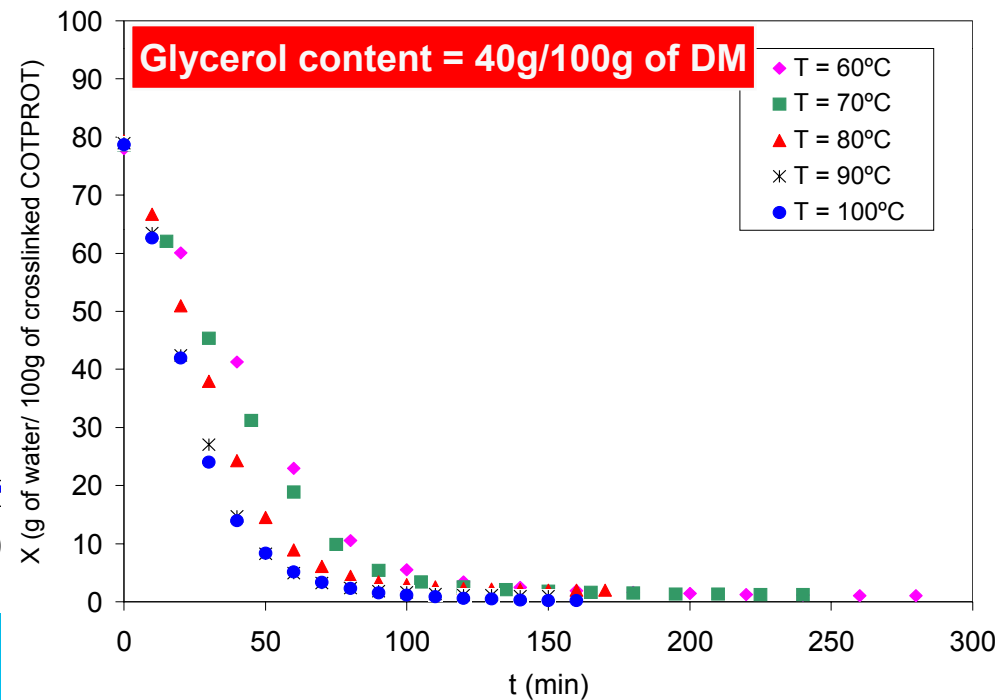
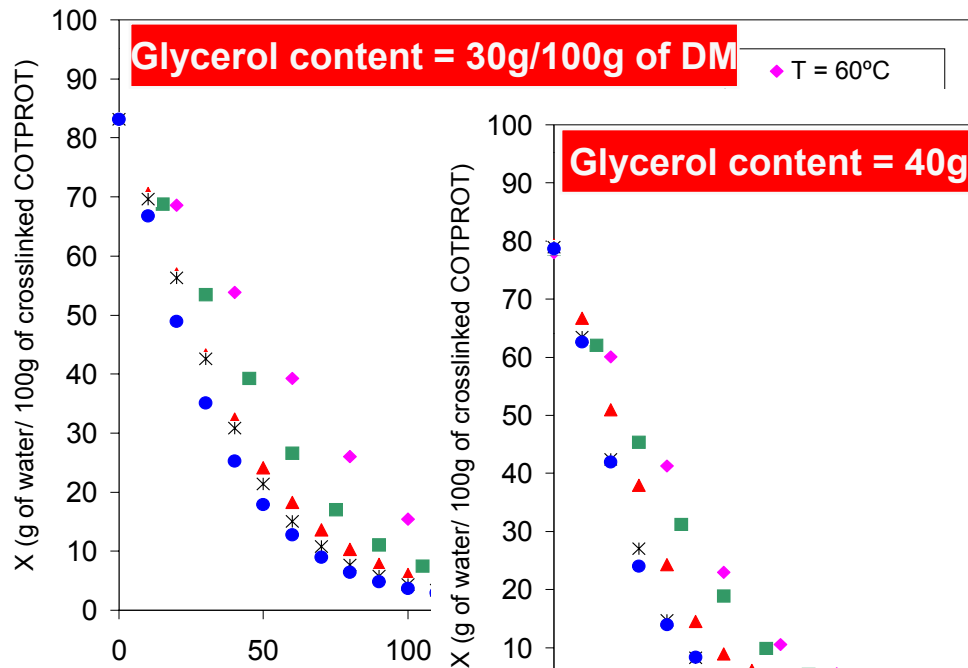
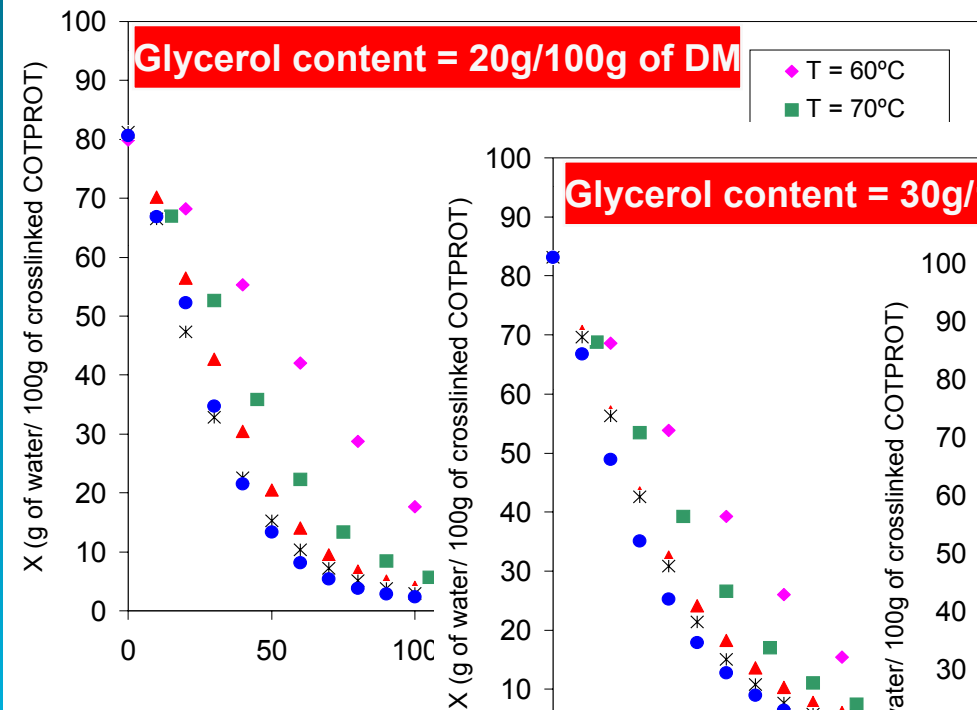


Glutaraldehyde/reactive lysine molar ratios of 6 ( $\diamond$ ) and 3 ( $\Delta$ )

# Choice of the support



# Drying the solution



# Characterization of films



# SPREAD COATING

INTI  Plásticos

# Spread Coating equipment

## Design and Construction

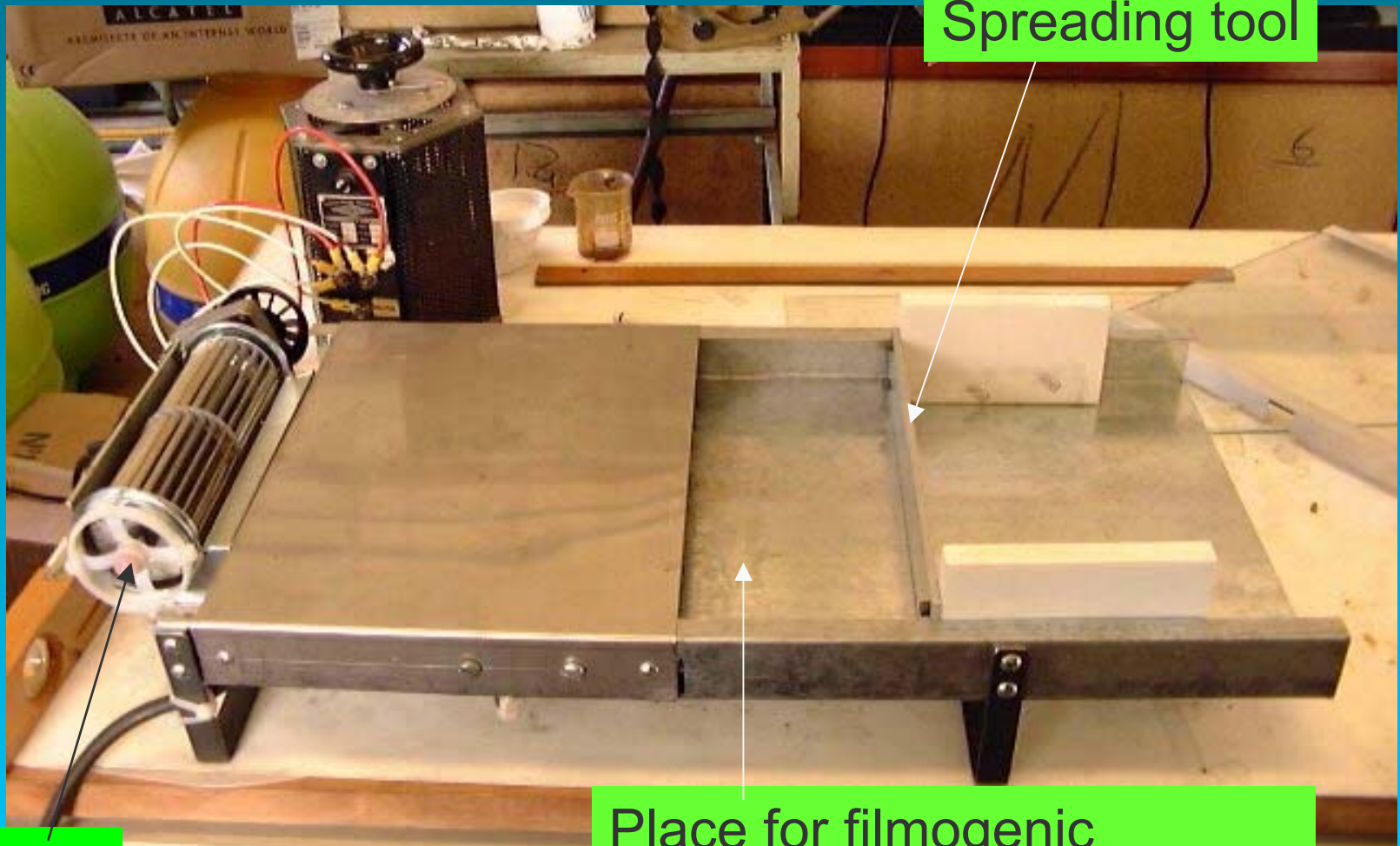
### Raw Material

- ➔ High viscous COTPROT solution adequate formulated

A prototype of the equipment was built in order to evaluated the film forming conditions.



# Spread coating equipment prototype



Ventilator

Spreading tool

Place for filmogenic solution



# Spread coating equipment prototype (results)

- The spread coating process was suitable for our formulation
- The formulation spread facility needs careful viscosity adjustment
- Drying conditions (time and temperature): the drying process needs to be very slow, at low temperature, in order to obtain a good film surface quality.

# Spread coating equipment prototype (results)

The results obtained with the prototype spread coating equipment allows us to determine:

- Pilot plant equipment dimensions (equipment length)
- Endless rubber blanket: design, material type and velocity regulation
- Drying system: type of system, conditions (air velocity)

# Film obtained with the prototype spread coating equipment



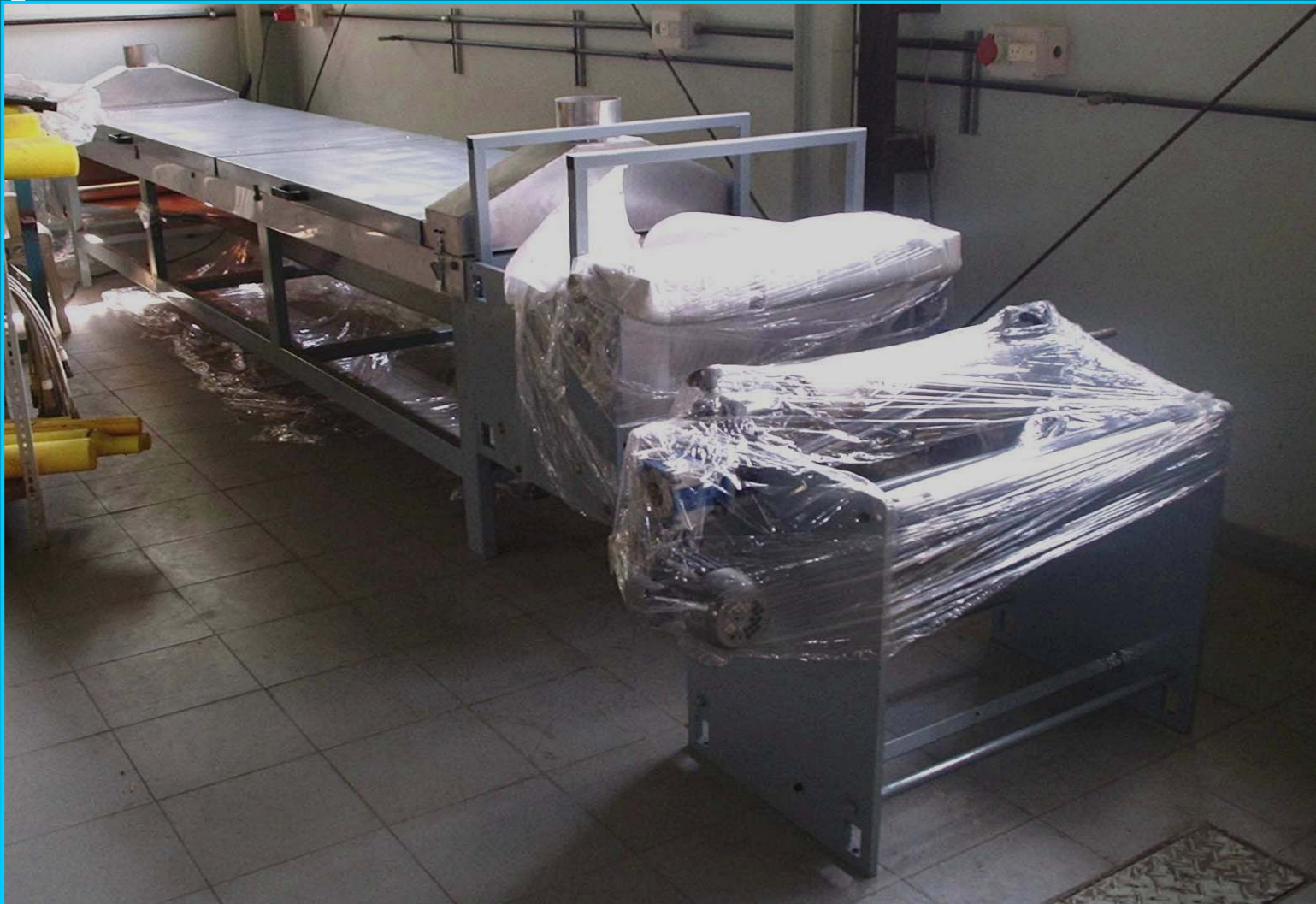
Film formulated with SDP; glutaraldehyde, glycerol and Polyvinyl alcohol (1.0 % w/w). Dried with the prototype spread coating equipment at 40°C , 1 h, 60°C 30 min

# Casting vs spread coating

## Film fabrication

Filmogenic Solution (FS)	Mass Area (mg/cm <sup>2</sup> )	Water content (%)	Thickness (mm)	Maximum Tensile Strength (MPa)	Maximum elongation (%)
DM:10%, Gly:20% Glu/RL:3.6 Casting	31.1	9.8 (SD=0.2)	0.27 (SD=0.04)	4.5 (SD:0.8)	51 (SD:22)
DM:10%, Gly:20% Glu/RL:3.6 Spread Coating	-	10.3 (SD=0.1)	0.17 (SD=0.01)	4.5 (SD:0.4)	84 (SD:19)

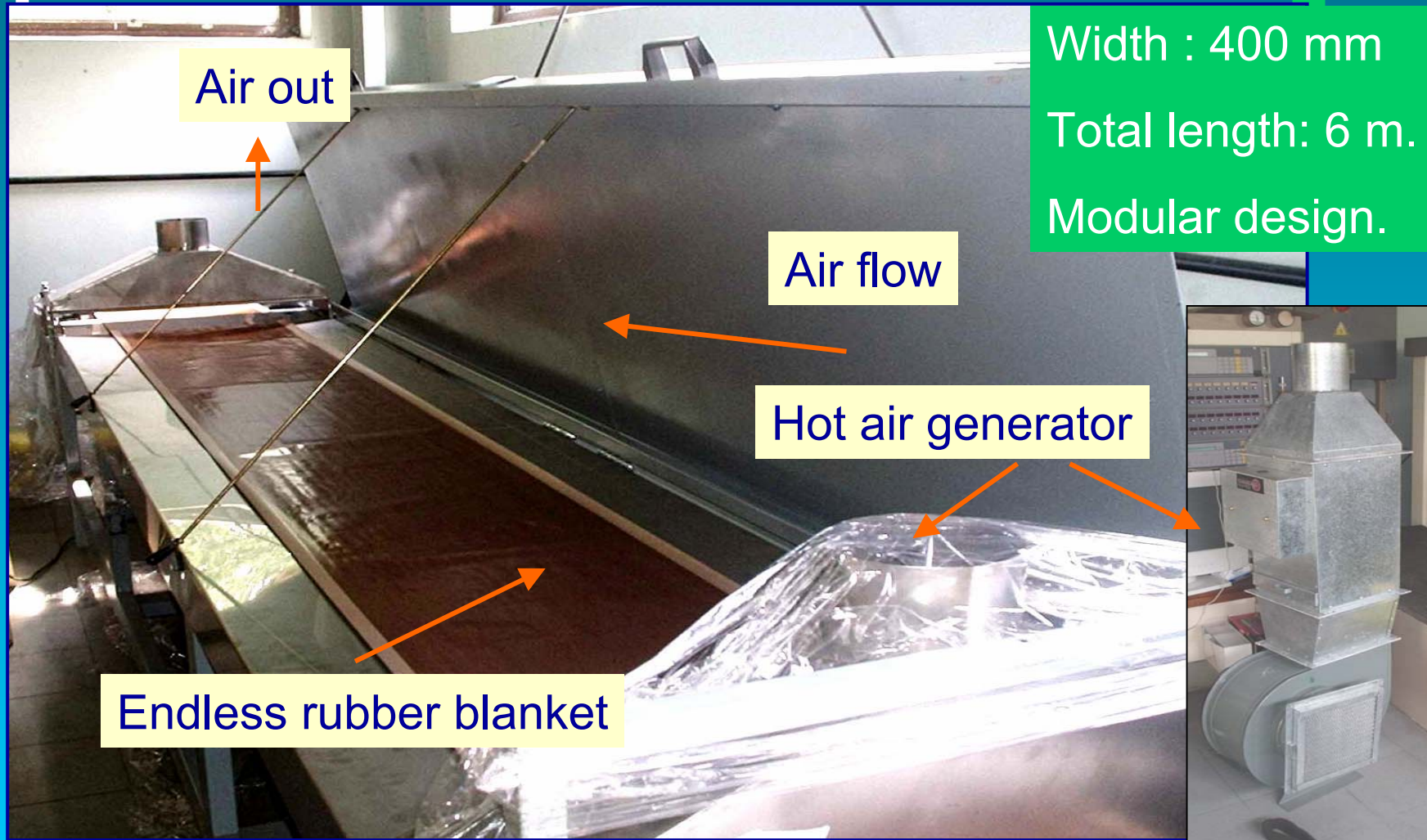
# Pilot plant spread coating equipment





# Pilot plant spread coating equipment

Width : 400 mm  
Total length: 6 m.  
Modular design.



# Pilot plant spread coating equipment





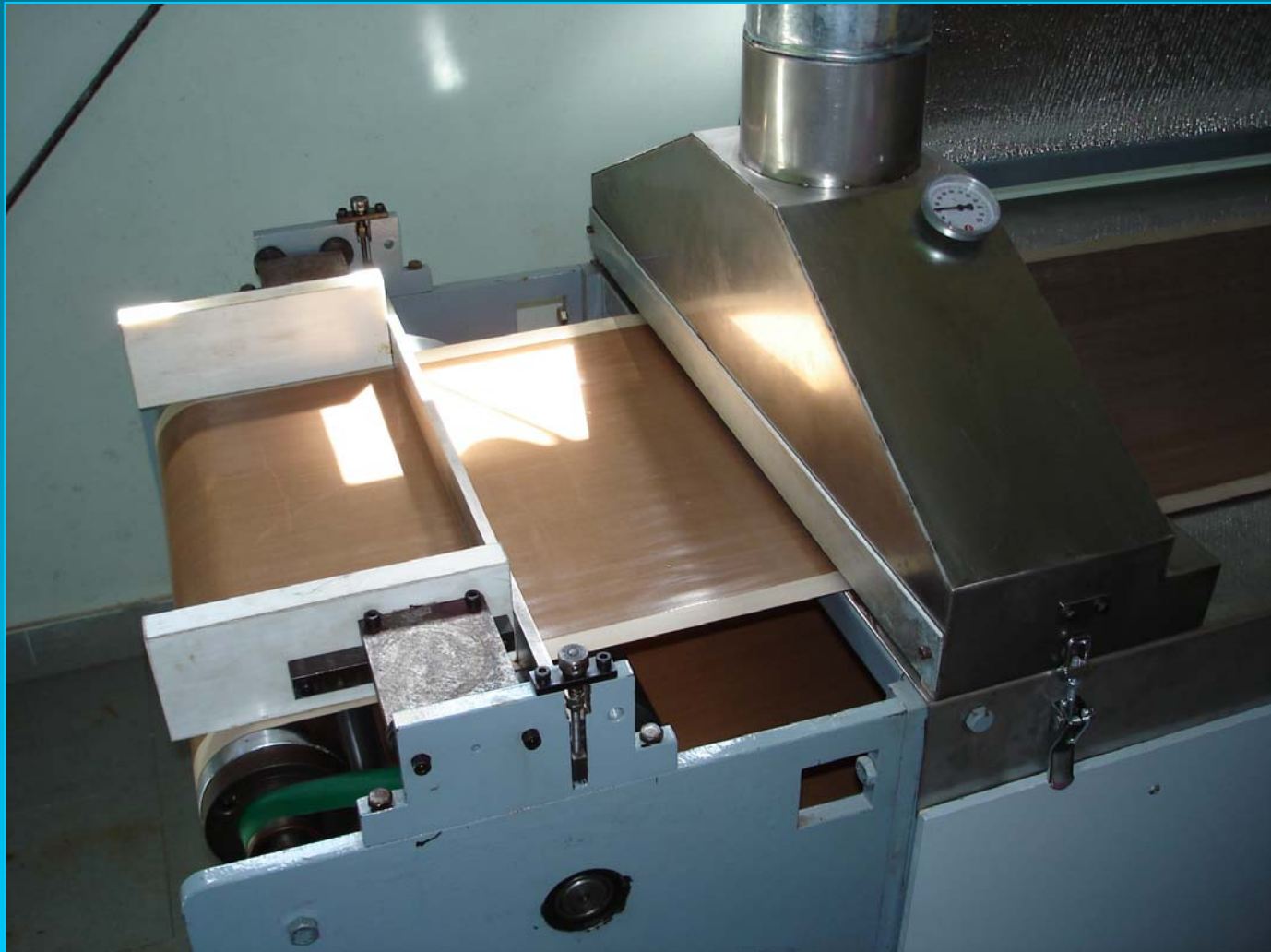
# Pilot plant spread coating equipment





# Spread coating equipment

## Spreading the film-forming solution



# Spread coating equipment

## Spreading the film-forming solution



# Spread coating equipment

## Non reinforced film fabrication

Film coming out from the  
drying zone

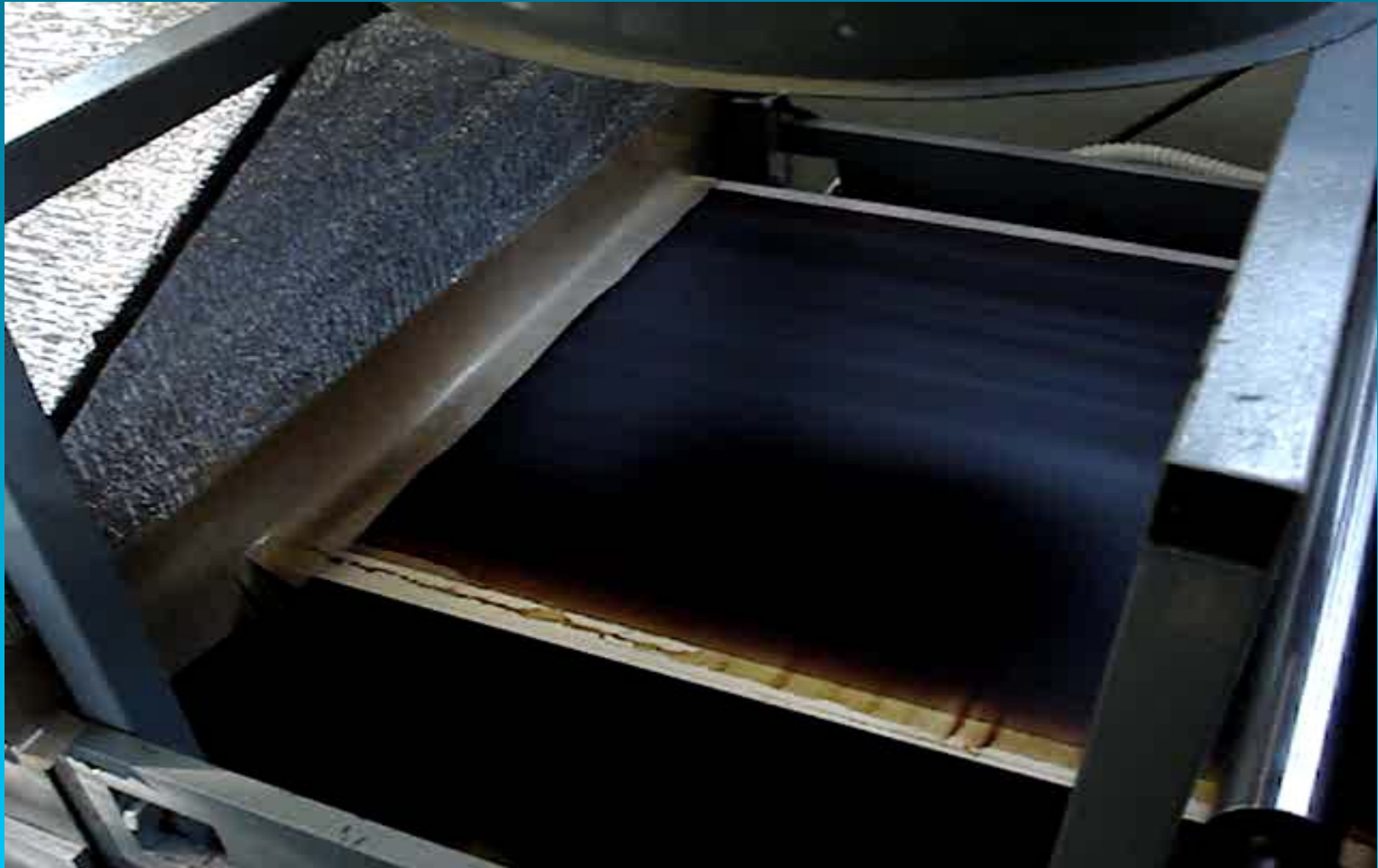


Film in the rolling system



# Spread coating equipment

## Non reinforced film fabrication





# Spread coating equipment

## Non reinforced film fabrication



# EXTRUSION – THERMOFOUDDING

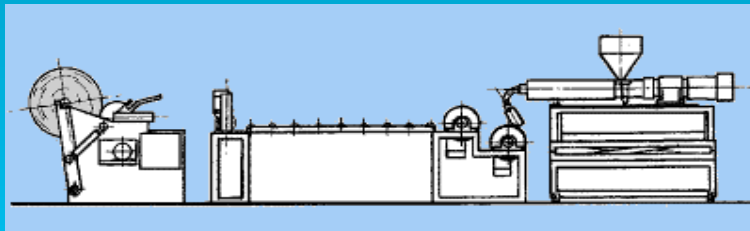


ÉCOLE DES MINES D'ALÈS  
Alès - Nîmes - Pau

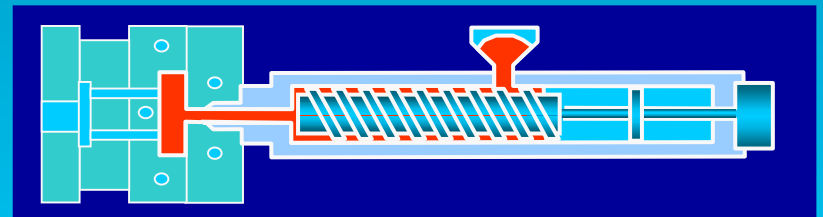
# Dry technologies

## ➔ Melt processing techniques

- ➔ Thermoplastic polymers
- ➔ Temperature and mechanical forces induce polymer flow
- ➔ Molten polymer is pushed :
  - Through a die (extrusion)
  - Into a mould (injection-moulding)



**Cast extrusion**



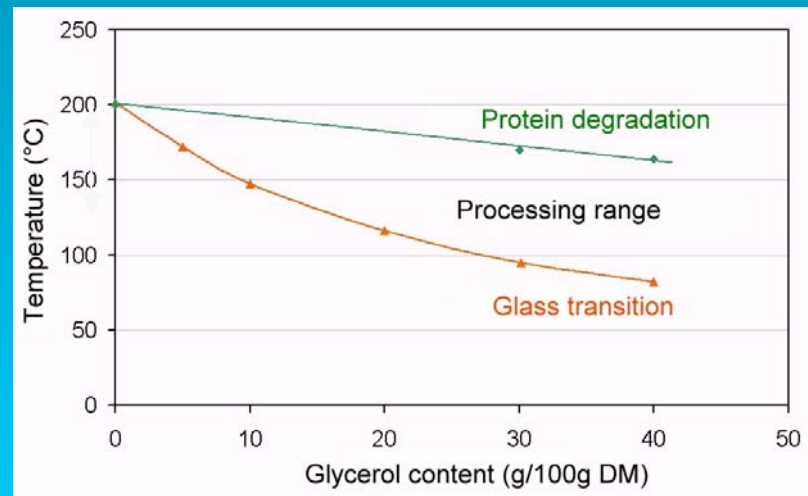
**Injection moulding**

# Processing proteins

## ➔ Requirements for dry processing

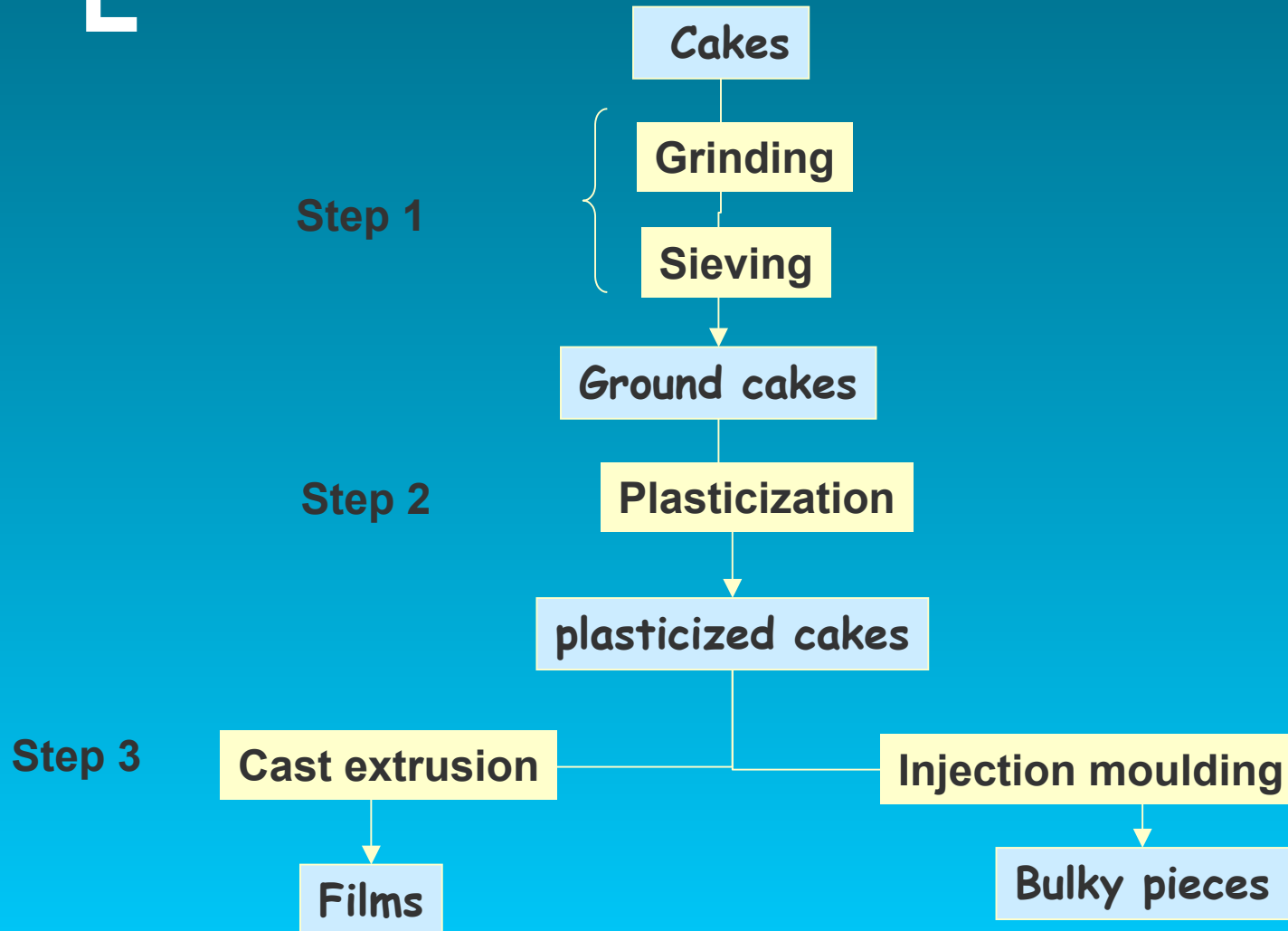
- ➔ Reach the « molten » state ( $T > T_g$ )
- ➔ Avoid protein degradation

## ➔ Necessity to use plasticizers to enlarge the processing range





# Scheme of the process



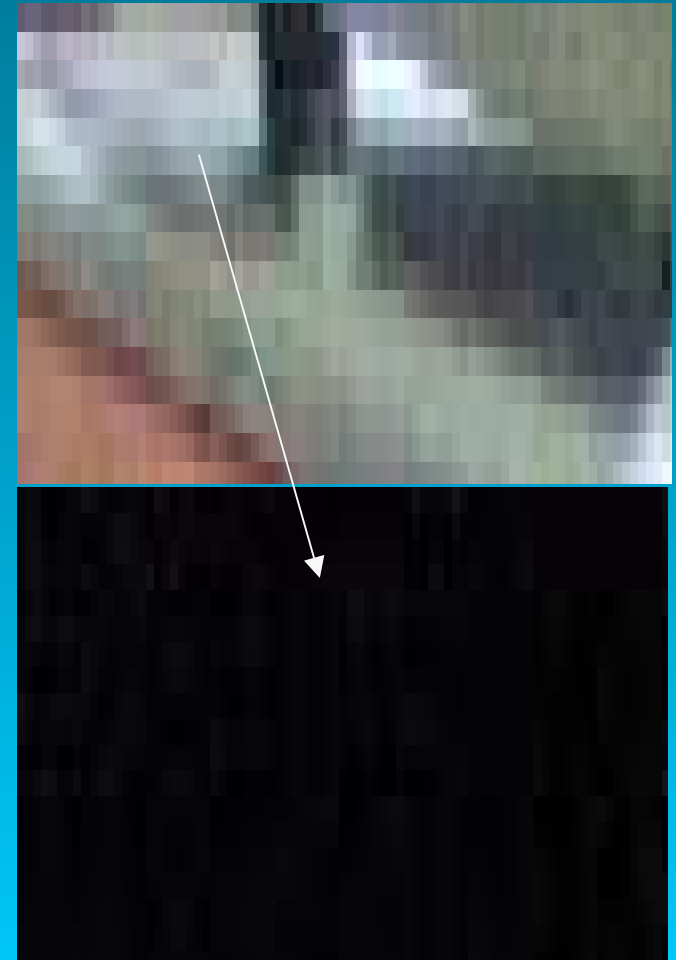
# Step 1

## ➔ Grinding

- ➔ Obtaining of fine powder to favorize further plasticization

## ➔ Sieving

- ➔ Obtaining a calibrating powder
- ➔ Elimination of shells and linter



# Step 1

- Protein enrichment
  - Delipidated Cakes



	Proteins	Lipids	Cellulose
Raw matter	<b>33.23</b>	<b>0.93</b>	<b>19.09-20.18</b>
Ground, sieved at 400 $\mu\text{m}$	<b>41.68</b>	<b>1.84</b>	<b>12.90-12.81</b>

(g/100g DM)

# Step 2

## ➔ Plasticization

### ➔ 3 plasticizers

- Glycerol ( $C_3H_8O_3$ ) 92 g/mol
- Triethanol amine ( $C_6H_{15}NO_3$ ) 149 g/mol
- Polyethylene glycol ( $HO-(CH_2CH_2O)_4-H$ ) 194 g/mol
- 0, 10, 20% w/w

## ➔ Processing at laboratory scale

### ➔ Internal mixer (Haake)

- Plasticizer is introduced at room temperature
- Progressive heating up to 90°C

### ➔ Thermocompression

- P = 50 bars
- T = 120°C



# Step 2

## ➔ Main results (presented tomorrow)

- ➔ Glycerol gives the best plasticizing effect
- ➔ 20% g/100 g DM content
- ➔ Presence of lipids in the powder must be avoided
- ➔ Presence of shells must be avoided
- ➔ Necessity to combine temperature and pressure to unfold cottonseed proteins

# Step 2

## ➡ Compounding at pilot scale

### ➡ Device

- Twin-screw extruder
- Peristaltic pump to introduce glycerol

### ➡ Processing conditions

- Screw profile
- Temperature profile
- Screw rotation speed



Step 2



# Step 3

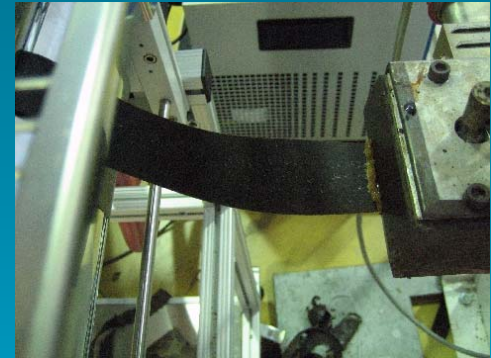
## → Cast extrusion

### → Devices

- Single screw extrusion
- Flat die
- Calender

### → Processing conditions

- Temperature profile
- Screw rotation speed
- Roll temperature





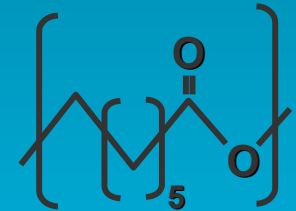
Step 3



# Step 3

## → Results of processing

- Possible with plasticized flours
- Difficult with plasticized cakes
- Interesting results by mixing plasticized cakes with PCL



Polycaprolactone (PCL)



# Step 3

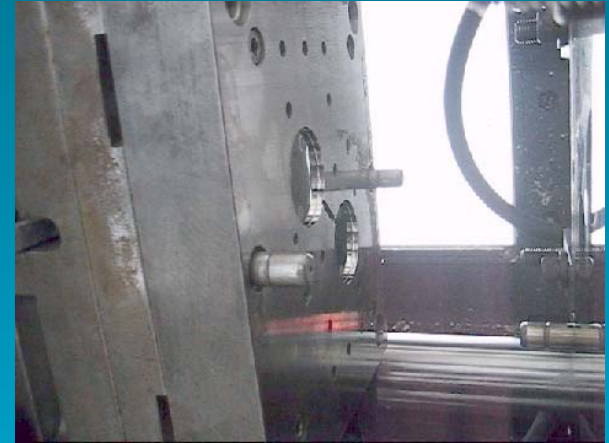
## ➔ Injection moulding

### ➔ Device

- Sandretto Press (95 t)
- Mould : disk

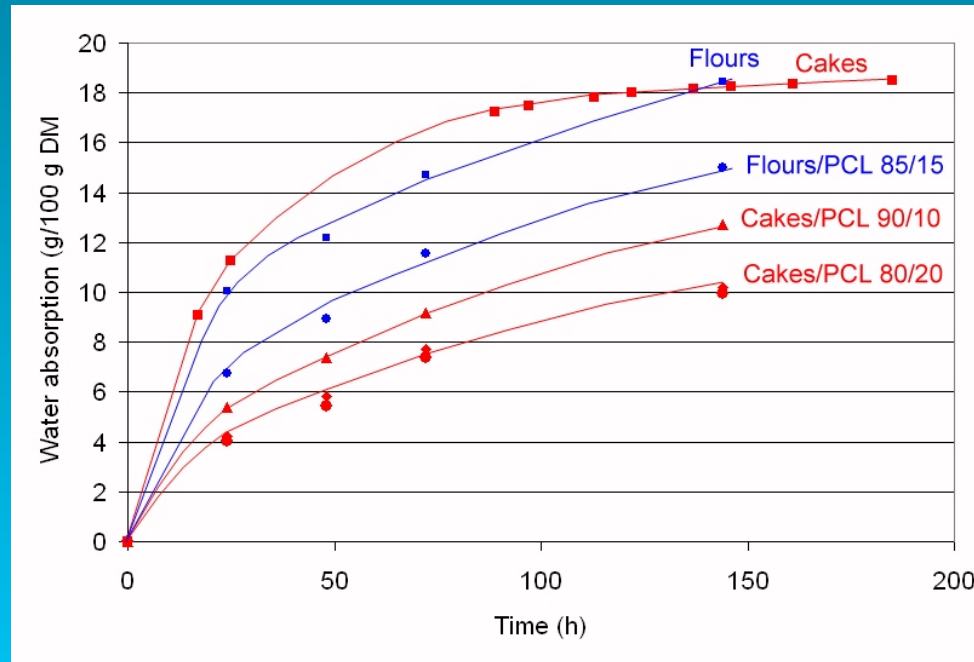
### ➔ Processing conditions

- Barrel temperature
- Mould temperature
- Pressure
- Cycle time



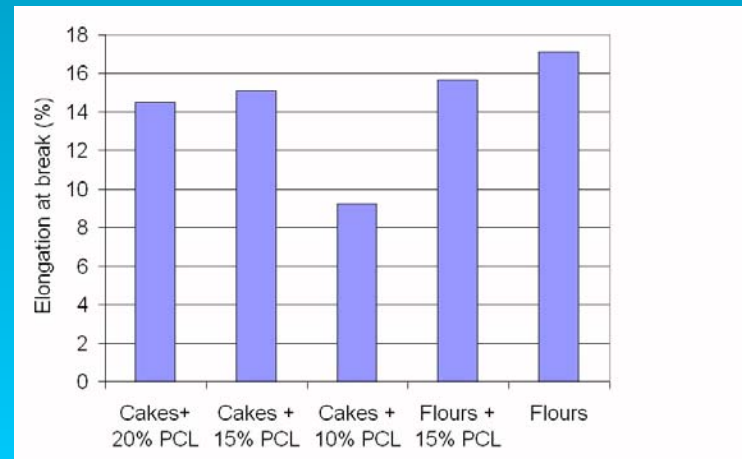
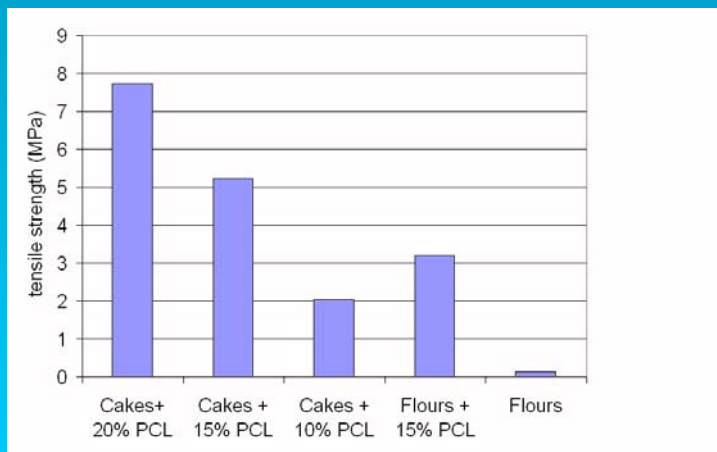
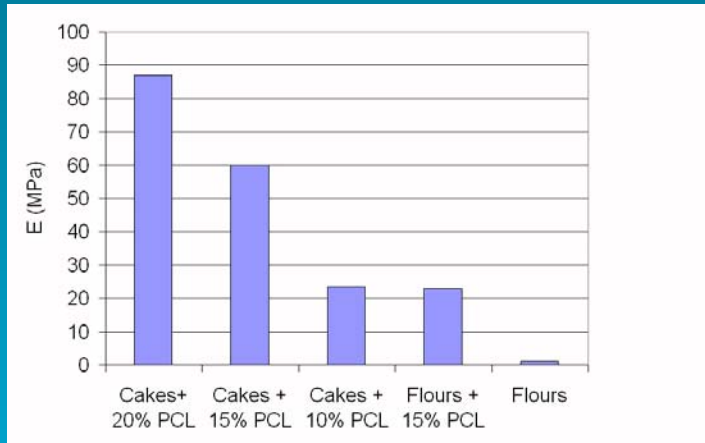
# Film properties

## → Hygroscopicity



# Film properties

## → Mechanical properties



# Conclusions

- ➡ Using different raw matters (cakes, flours) we showed the feasibility of making films and sheets by standard polymer processing techniques :
  - ➡ Casting
  - ➡ Spread coating
  - ➡ Extrusion

# Conclusion about spread coating

Necessity :

- ➡ to adjust viscosity in order to obtain good film processability
- ➡ to obtain homogeneous film thickness



# Conclusion about extrusion and injection moulding

- ➔ Necessity to improve plasticized cakes cohesion (adding PCL)
- ➔ Necessity to decrease shell content
- ➔ Necessity to use delipidated matter (solvent extraction)

