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1 Effect of torrefaction pretreatment on the pyrolysis of rubber wood sawdust analyzed by

2 Py-GC/MS

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15 Abstract

16 The aim of this study was to investigate the effect of torrefaction on the pyrolysis of
17 rubber wood sawdust (RWS) using pyrolysis–gas chromatography/mass spectrometry
18 (Py-GC/MS). Three typical torrefaction temperatures (200, 250, and 300 °C) and pyrolysis
19 temperatures (450, 500, and 550 °C) were considered. The results suggested that only diethyl
20 phthalate, belonging to esters, was detected at the torrefaction temperatures of 200 and 250 °C,
21 revealing hemicellulose degradation. With the torrefaction temperature of 300 °C, esters,
22 aldehydes, and phenols were detected, suggesting the predominant decomposition of
23 hemicellulose and lignin. The double-shot pyrolysis indicated that the contents of
24 oxy-compounds such as acids and aldehydes in pyrolysis bio-oil decreased with rising
25 torrefaction temperature, implying that increasing torrefaction severity abated oxygen content
26 in the bio-oil. With the torrefaction temperature of 300 °C, relatively more cellulose was
27 retained in the biomass because the carbohydrate content in the pyrolysis bio-oil increased
28 significantly.

29 **Keywords:** Torrefaction; Pyrolysis; Bio-oil; Py-GC/MS; Double-shot analysis.

30

31 1. Introduction

32 In recent years, renewable energy has become of growing interest. Biomass is considered
33 as an important renewable fuel and can be processed into other forms of fuel through
34 thermochemical conversion processes such as torrefaction, pyrolysis, gasification, and
35 liquefaction (Chen et al., 2011; Kumar et al., 2017). Pyrolysis converts biomass via thermal
36 degradation in an oxygen-free condition at temperatures between 400 and 650 °C. This results
37 in the production of bio-oils, various gaseous components, and non-volatiles which are further
38 collected as biochars (Bridgwater, 2012). The pyrolytic products include a variety of
39 chemicals such as alkanes, aromatic, hydrocarbons, phenol derivatives, and a few ketones,
40 esters, ethers, sugars, amines, alcohols, etc. It is essential to understand the mechanisms of
41 product formation during the rapid pyrolysis of biomass inasmuch as this can provide the
42 basic information for the selective pyrolysis process to obtain high-grade bio-oils (Chen &
43 Lin, 2016).

44 One of the potential ways to decrease the oxygen content and improve the quality of
45 bio-oil is to pretreat biomass at a temperature range of 200-300 °C, under atmospheric
46 pressure, and in an inert atmosphere termed torrefaction (Chen et al., 2016; Kumar et al.,
47 2017). Zheng et al. (2014) found that increasing torrefaction temperature of pine wood from
48 220 to 280 °C decreased the bio-oil yield, but the oxy-compound contents such as acids and
49 aldehydes decreased sharply, while the aromatic hydrocarbon contents increased significantly,
50 leading to an increase in the heating value of bio-oil. Wigley et al. (2016) pretreated wood
51 chips via torrefaction, and found that the char yield was higher following torrefaction and the
52 bio-oil from torrefied biomass was slightly enriched in levoglucosan and aromatics compared
53 to raw bio-oil.

54 A novel technique to investigate the evolution of the components in biomass in the
55 course of pyrolysis is the pyrolysis–gas chromatography/mass spectrometry (Py-GC/MS).

56 Py-GC/MS is an important technique for biomass characterization because it can detect
57 pyrolytic products effectively through the comparison of the total chromatographic peak areas
58 obtained at different conditions during the pyrolysis process (Gao et al., 2013). Regarding the
59 applications of Py-GC/MS, Gu et al. (2013) analyzed pyrolysis mechanisms of poplar wood at
60 600 °C. They proposed that the pyrolytic mechanism of cellulose and hemicellulose was from
61 depolymerization to anhydrosugars and furans or pyranose ring-breaking to light oxygenated
62 species, while the thermal degradation of lignin formed aromatic hydrocarbons. Zhang et al.
63 (2016) discussed the effect of torrefaction pretreatment at two different temperatures (250 and
64 280 °C) on the pyrolysis products from rice husk. They underlined that the pretreatment
65 decreased the contents of acids, ketones, aldehydes and furans, but significantly increased the
66 contents of sugars, especially levoglucosan. Yang et al. (2014) addressed the effect of
67 torrefaction on switch grass pyrolysis products. Compared to the pyrolysis products of raw
68 switch grass, the contents of anhydrous sugars and phenols in the pyrolysis products of
69 torrefied switch grass were higher. When the torrefaction temperature increased from 230 to
70 270 °C, the contents of anhydrous sugars and phenols in pyrolysis products increased,
71 whereas the contents of guaiacols decreased.

72 In recent years, many researches have been carried out on torrefaction pretreatment to
73 improve biomass properties (Chen et al., 2015b), and a few studies have been conducted on
74 the biomass torrefaction followed by pyrolysis, namely, the two-stage thermochemical
75 conversion process. The examination of the literature suggests that Py-GC/MS is a potential
76 tool to investigate the thermal degradation mechanisms of biomass. Though the pyrolysis
77 phenomena of torrefied biomass have been reported in some studies, it should be illustrated
78 that, to date, no research has been carried out on the integration of biomass torrefaction and
79 pyrolysis analyzed by Py-GC/MS. For this reason, the present study aimed to examine the
80 effects of different torrefaction pretreatment temperatures on biomass pyrolysis characteristics.
81 To achieve this target, the thermal degradation behaviors of rubber wood sawdust (RWS) at

82 different combinations of torrefaction temperatures and pyrolysis temperatures were
83 investigated where a two-stage process using a double-shot pyrolyzer was practiced. In this
84 way, there was no need to interrupt the process when the first stage was completed, and the
85 experiment could directly proceed to the second stage. The detailed information of product
86 formations and reaction mechanisms from the biomass torrefaction followed by pyrolysis was
87 clearly figured out.

88 2. Experimental

89 2.1. Raw material and analysis

90 The raw material used in this study was rubber wood sawdust (RWS), which was
91 obtained from CPC Corporation in Taiwan. The biomass was meshed to sizes less than 1.7
92 mm, followed by drying in an oven at 105 °C for 24 h to remove moisture. Thereafter, it was
93 stored in sealed plastic bags and placed in a desiccator until experiments were carried out. In
94 the fiber analysis, hemicellulose, cellulose, and lignin contents in the raw RWS were
95 measured, following the method adopted previously (Chen et al., 2010). The analysis
96 indicated that hemicellulose, cellulose, and lignin contents in the RWS were 26.28, 49.14,
97 13.44 wt%, respectively.

98 2.2. Py-GC/MS system

99 The entire system of Py-GC/MS was made up of a pyrolyzer (EGA/PY3030D) and a gas
100 chromatography/mass (GC/MS) spectrometer (Agilent Technologies 7890A/5975C). A
101 two-stage thermal degradation of the RWS by use of a double-shot pyrolyzer was practiced.
102 The pyrolyzer was coupled with the GC/MS to separate and identify the volatiles liberated
103 from the RWS. An ultra-alloy capillary column (30 m–0.25 mm–0.25 μm) was applied in the
104 GC/MS system. The oven temperature was set as follows: (1) 45 °C for 4 min; (2) from 45 to
105 240 °C at a heating rate of 6 °C min^{-1} ; and (3) the capillary column was maintained at 240 °C
106 for about 5 min. High-purity helium at a flow rate of 1.0 mL min^{-1} was used as the carrier gas

107 and sent into the reaction system. The injector and interface temperatures in the GC/MS were
108 held at 275 and 300 °C, respectively, to identify the pyrolysis volatiles. The mass range used
109 for the mass selective detector was 40–550 m/z. The detected products were identified
110 through a comparison between the experimental mass spectrum and the mass spectrum library
111 attached to the Py-GC/MS apparatus (Wang et al., 2016). To ascertain the measurement
112 quality of the Py-GC/MS system, it was periodically calibrated. Moreover, prior to the
113 experiments certain samples were tested at least twice. The results showed high
114 reproducibility and consistency, revealing the reliability of the measurements.

115 2.3. Py-GC/MS experimental procedure

116 In the experiments, three different torrefaction temperatures of 200, 250, and 300 °C,
117 corresponding to light, mild, and severe torrefaction, respectively, were taken into account.
118 Meanwhile, three typical pyrolysis temperatures of 450, 500, and 550 °C (Chen & Lin, 2016)
119 were considered. In each experimental run, about 0.2 mg of the RWS was loaded in a crucible.
120 Then, the crucible was held by a hook to fix its position in the pyrolysis tube. Before the
121 pyrolyzer reached the desired torrefaction temperature, the biomass loaded in the crucial was
122 suspended beyond the pyrolyzer. Once the torrefaction temperature was reached, the crucible
123 was sent into the pyrolyzer for 10 min for the first stage reaction, and produced volatiles were
124 separated and identified by the GC/MS. Afterward, the crucial backed to the location beyond
125 the pyrolyzer. When the pyrolyzer reached the desired pyrolysis temperature, the crucible was
126 sent into the pyrolyzer again for the second stage reaction for 2 min. The produced volatiles
127 were analyzed by the GC/MS (Lee et al., 2005), accomplishing the two-stage reaction.

128 3. Results and discussion

129 3.1. Single-shot pyrolysis

130 In the pyrogram of the RWS pyrolyzed at 500 °C where the abundance of each product
131 was obtained via the Py-GC/MS detected peak area divided by the sample mass, more than 50

132 peaks were found (E-Supplementary data for this work can be found in e-version of this paper
133 online), and the main compounds, including acids, phenols, ketones, aldehydes, alcohols,
134 carbohydrates, and esters, were listed in **Table 1**. The prime pyrolytic products of the RWS
135 were classified into five groups: acids, phenols, ketones, aldehydes, and carbohydrates. Their
136 weight percentages were 5.38, 14.99, 2.71, 5.64, and 19.25 wt%, respectively. Meanwhile, the
137 principal components contained in pyrolysis volatiles from the RWS have diethyl phthalate,
138 2,6-dimethoxy-4-allylphenol, coniferyl aldehyde, etc (E-Supplementary data for this work can
139 be found in e-version of this paper online). The acids such as acetic acid (peak #5) (Wenzel,
140 1970) and the ketones such as 2-cyclopenten-1-one, 2-hydroxy- (peak #6) (Zhao et al., 2016)
141 were assigned to hemicellulose degradation. The phenols such as 2,6-dimethoxy-4-allylphenol
142 (peak #2), 2-methoxy-4-methylphenol (peak #7), 2-methoxy-4-vinylphenol (peak #9),
143 syringol (peak #10), and isoeugenol (peak #12) (Liu et al., 2016) and the aldehydes such as
144 2,5-dimethoxy-4-methylbenzaldehyde (peak #15) (Arias et al., 2006) were due to lignin
145 degradation. The carbohydrates such as D-Allose (peak #13) and
146 1,6-anhydro-beta-d-glucopyranose (peak #14) stemmed from cellulose degradation (2017). In
147 the fiber analysis, cellulose accounted for 49.14 wt%. This might be the reason why the
148 weight percent of the carbohydrates was the highest among all the species of volatiles.

149 3.2. *Double-shot pyrolysis*

150 3.2.1. *First stage torrefaction of double-shot pyrolysis*

151 The TICs of the RWS torrefied at three different temperatures (i.e., 200, 250, and 300 °C)
152 in the first stage suggested that only one peak (#1), namely, diethyl phthalate which pertained
153 to esters, appeared in the pyrograms at the torrefaction temperatures of 200 and 250 °C
154 (E-Supplementary data for this work can be found in e-version of this paper online). The
155 content of diethyl phthalate almost accounted for 100 wt% in the gaseous product from the
156 RWS torrefaction. No other peak signals were observed in the torrefaction pyrograms. This
157 was probably because the biomass was less active at lower torrefaction temperatures, whereby

158 fewer organic compounds were converted into volatiles (Font Palma, 2013). As described
159 earlier, esters were produced from the thermal degradation of hemicellulose. Accordingly, it
160 was recognized that the single peaks were due to the thermal decomposition of hemicellulose
161 in the RWS (E-Supplementary data for this work can be found in e-version of this paper
162 online). This result was consistent with other studies (Chen & Kuo, 2010; Chen & Kuo, 2011)
163 in which it was underlined that torrefaction had the most profound impact upon hemicellulose
164 when compared with cellulose and lignin. Wenzel (Wenzel, 1970) also highlighted that esters
165 were released from hemicellulose decomposition at 150-300 °C. With the torrefaction
166 temperature of 300 °C, on the other hand, more volatile products in the pyrograms were
167 observed (E-Supplementary data for this work can be found in e-version of this paper online),
168 and their relative peak areas were listed in **Table 2**. It could be seen that aldehydes such as
169 coniferyl aldehyde (peak #3) and 3,5-dimethoxy-4-hydroxycinnamaldehyde (peak #4),
170 phenols such as 2,6-dimethoxy-4-allylphenol (peak #2), isoeugenol (peak #12), and esters
171 such as diethyl phthalate (peak #1) were the most prominent products in that their weight
172 percentages in the torrefaction product were 19.53, 9.58, and 35.15 wt%, respectively. In
173 **Table 2**, coniferyl aldehyde was responsible to 42.85% of the aldehyde volatiles. This agreed
174 with the observation of Arias et al. (2006) where it was reported that the major signal in
175 pyrograms at temperatures of 250 and 300 °C was coniferyl aldehyde, resulting from the
176 thermal decomposition of lignin. Rousset et al. (2009) also studied lignin structure at 280°C
177 using thioacidolysis method and showed intense structural transformations with the following
178 degradation reactions: (1) the cleavage of lignin β -O-4 bonds; (2) a severe recondensation
179 reactions, which led to considerable enrichment of resistant interunit bonds in the
180 thermally-treated lignin; (3) the formation of vinyl ether structures through the loss of the
181 terminal hydroxymethyl groups from lignin sidechains; the liberated formaldehyde then
182 participated in crosslinking the polymer according to similar mechanisms to those of
183 heat-hardened formo-phenolic resins; and (4) to a lesser extent, the oxidative cleavage of the

184 C α -C β benzylic bonds with the formation of benzoic acid and benzoic aldehyde end-groups in
185 lignin. By virtue of notable production of esters, aldehydes, and phenols, it followed that the
186 formation of volatiles was owing to predominant decomposition of hemicellulose and lignin
187 at this temperature (i.e., 300 °C). In contrast, carbohydrates such as
188 1,6-anhydro-beta-d-glucopyranose (peak #14) merely accounted for 3.07 wt%. This implied,
189 in turn, that the thermal decomposition of cellulose in the RWS was not pronounced. Overall,
190 the pyrograms at 200, 250, and 300 °C (E-Supplementary data for this work can be found in
191 e-version of this paper online), qualitatively agreed with the observations of Chen et al. (2011)
192 where they observed that the GC/MS spectra of the condensed liquids from Lauan torrefied at
193 200 and 250 °C were similar to each other, whereas there was a notable difference in the
194 spectrum at 300 °C from the preceding two temperatures.

195 3.2.2. *Second stage pyrolysis of double-shot pyrolysis*

196 A comparison to the pyrogram of single stage reaction indicated that less peaks were
197 detected in multiple stage reaction (E-Supplementary data for this work can be found in
198 e-version of this paper online), especially for those at longer retention time (> 30 min) where
199 the peaks of aldehydes (e.g., peaks #3, 4, 15, 16), stemming from lignin degradation (Arias et
200 al., 2006), in the pyrograms were abated. This was presumably attributed to some components
201 in the biomass being preliminarily decomposed from torrefaction so as to produce less
202 compounds from the second stage pyrolysis. The comparison between the three figures of the
203 multiple stage reaction (E-Supplementary data for this work can be found in e-version of this
204 paper online), suggested that the number of peaks had a trend to diminish when the retention
205 time was larger than 25 min, especially for the pyrolysis of the biomass torrefied at 300 °C.
206 An increase in torrefaction temperature intensified lignin decomposition. This was the reason
207 why the peaks of phenols (e.g., peaks #7, 8, 9, 10, 12) at the retention time of 23-30 min
208 decreased at higher torrefaction temperatures. This reflected that torrefaction was able to
209 make the properties of the biomass more uniform so that relatively less compounds were

210 generated from its pyrolysis. In summary, the pyrolytic product distributions from the RWS
211 changed to a certain extent when torrefaction was applied, especially under severe torrefaction.
212 This behavior was also observed by Wang et al. (2017) who examined the pyrolysis behavior
213 of cellulose through GC/MS analysis.

214 The relative contents of different groups of chemicals (i.e., acids, phenols, ketones,
215 aldehydes, and carbohydrates) from the pyrolysis of the torrefied RWS are profiled in **Fig. 1a**
216 where the chemicals produced from the single stage pyrolysis are also shown for comparison.
217 Acids were a major constituent of the volatiles produced from hemicellulose pyrolysis. An
218 increase in torrefaction temperature intensified the thermal degradation of hemicellulose. This
219 the reason why a decent in acid content was exhibited when the torrefaction temperature went
220 up where the acetic acid was the prime constituent in the acids (**Table 1**). Phenols and
221 aldehydes were the main pyrolytic products from the thermal degradation of lignin.
222 Torrefaction also had an impact upon lignin decomposition (Chen et al., 2015). Phenols and
223 aldehydes had a trend to decrease with rising torrefaction temperature, revealing that lignin in
224 the RWS was also sensitive to the torrefaction temperature. It was known that oxy-compounds
225 such as acids and aldehydes might cause bio-oil instability. Their yields decreased with
226 increasing torrefaction temperature, implying that increasing torrefaction severity could abate
227 the oxygen content and improve bio-oil quality (Wigley et al., 2016). The decrease in phenols
228 under higher torrefaction temperatures was in line with the result of Gogoi et al. (2017) where
229 they pointed out that an increase in torrefaction temperature and time might decrease the yield
230 of phenols, resulting from lignin decomposition and carbonization during the torrefaction
231 process. As for the cellulose in the RWS, the influence of torrefaction at 250 °C upon
232 cellulose was more than that at 200 °C. As a consequence, relatively more cellulose was
233 retained in the torrefied biomass at 200 °C and the carbohydrate content in the pyrolytic
234 product was higher. With regard to the RWS undergoing torrefaction at 300 °C, the

235 carbohydrate content was by far higher than the other biomass samples, presumably due to
236 higher thermal resistance of cellulose at 300 °C when compared to hemicellulose and lignin.

237 3.3. Different combinations of torrefaction and pyrolysis temperatures

238 To proceed farther into the recognition of the formation characteristics of pyrolytic
239 products from torrefied biomass, three different combinations of torrefaction and pyrolysis
240 temperatures, namely, (torrefaction, pyrolysis) = (200 °C, 450 °C), (250 °C, 500 °C), and (300
241 °C, 550 °C), were taken into consideration, and their pyrograms (E-Supplementary data for
242 this work can be found in e-version of this paper online), were compared with each other.
243 Upon inspection of the pyrograms, the number of peaks decreased with increasing combined
244 temperatures when the retention time was longer than 25 min. This behavior was similar to
245 the pyrograms observed earlier. It followed that the torrefaction temperature played a
246 pronounced role on the pyrolysis of the RWS, regardless of the pyrolysis temperature. An
247 examination on the relative contents of the five different groups of compounds shown in **Fig.**
248 **1b** suggested that phenols and carbohydrates accounted for the larger shares in the pyrolytic
249 products. This revealed that relatively more lignin and cellulose were retained in the torrefied
250 biomass, especially for cellulose in the biomass torrefied at 300 °C. A comparison between
251 **Fig. 1a** and **Fig. 1b** at the torrefaction temperature of 200 °C indicated that produced
252 carbohydrates at the pyrolysis temperature of 450 °C had a lower yield (15.29 wt%, **Fig. 1b**)
253 than the pyrolysis temperature of 500 °C (18.37 wt%, **Fig. 1a**). This could be explained by
254 less cracking of cellulose in the course of pyrolysis. Alternatively, with the torrefaction
255 temperature of 300 °C, the produced carbohydrates at the pyrolysis temperature of 500 °C had
256 a higher yield (26.81 wt%, **Fig. 1a**) than the pyrolysis temperature of 550 °C (23.7 wt%, **Fig.**
257 **1b**), presumably due to more products formed from lignin degradation in the latter. The entire
258 profiles of phenols and carbohydrates in **Fig. 1b** were similar to those in **Fig. 1a**. This implied,
259 in turn, that torrefaction played a pivotal role in producing chemicals from biomass pyrolysis.

260 4. Conclusions

261 The Py-GC/MS analysis suggested that hemicellulose in the RWS was obviously
262 degraded from the torrefaction at 200 and 250 °C, and lignin decomposition was also
263 pronounced at 300 °C. The double-shot technique further indicated that the contents of acids
264 and aldehydes in pyrolysis vapor decreased with rising torrefaction temperature, and the
265 pyrograms depicted that less compounds were contained in the pyrolysis bio-oils. This
266 revealed that torrefaction could make bio-oil more uniform and reduce its oxygen content.
267 Carbohydrates in pyrolysis vapor increased significantly from the biomass torrefied at 300 °C,
268 implying that more cellulose was retained in the torrefied biomass.

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340 **Table 1.** Relative peak area distribution of the main products for biomass in Py-GC/MS

Bio-oil fraction	Formula	Relative content (%)						
		Single stage 500 °C	Two stage			250 °C 500 °C	300 °C	
			200 °C 450 °C	500 °C	500 °C		500 °C	550 °C
Acid	Acetic acid	$C_2H_4O_2$	5.38	10.71	8.10	7.11	6.11	7.59
Phenols	Phenol, 2-methyl-	C_7H_8O	0.11	1.08	-	0.44	-	-
	Phenol, 4-methyl-	C_7H_8O	0.24	-	-	0.42	-	-
	Phenol, 2-methoxy-	$C_7H_8O_2$	0.81	-	2.65	2.94	1.92	-
	2-Methoxy-4-methylphenol	$C_8H_{10}O_2$	0.90	1.78	2.14	2.41	2.49	1.25
	3-Methoxycatechol	$C_7H_8O_3$	1.43	2.08	-	1.20	1.71	1.50
	4-Ethyl-2-methoxyphenol	$C_9H_{12}O_2$	0.42	0.49	-	0.60	0.52	-
	2-Methoxy-4-vinylphenol	$C_9H_{10}O_2$	1.34	1.85	2.40	1.77	1.52	0.90
	Syringol	$C_8H_{10}O_3$	1.68	2.37	1.30	3.68	3.18	3.47
	4-((1E)-3-Hydroxy-1-propenyl)-2-methoxyphenol	$C_{10}H_{12}O_3$	1.94	0.44	6.08	-	-	-
Ketones	2-Cyclopenten-1-one, 2-hydroxy-	$C_5H_6O_2$	1.25	1.71	1.85	2.20	1.83	2.38
	1,2-Cyclopentanedione, 3-methyl-	$C_6H_8O_2$	-	-	-	1.12	0.76	-
Aldehydes	Butanedial	$C_4H_6O_2$	-	-	1.34	-	1.12	1.61
	Furfural	$C_5H_4O_2$	0.72	0.99	-	0.99	0.94	-
	Vanillin	$C_8H_8O_3$	0.73	0.35	0.71	0.36	-	-
	2,5-Dimethoxy-4-methylbenzaldehyde	$C_{10}H_{12}O_3$	1.59	-	1.84	2.96	-	2.76
	3,5-Dimethoxy-4-hydroxybenzaldehyde	$C_9H_{10}O_4$	1.10	0.78	2.89	0.56	0.36	-
	3,5-Dimethoxy-4-hydroxycinnamaldehyde	$C_{11}H_{12}O_4$	0.92	1.09	0.85	0.19	-	-
Carbohydrates	1,4:3,6-Dianhydro- α -d-glucopyranose	$C_6H_8O_4$	0.51	0.38	-	0.39	0.47	0.58
	D-Allose	$C_6H_{12}O_6$	14.37	14.91	15.92	3.93	25.09	23.12
	1,6-anhydro-beta-d-glucopyranose	$C_6H_{10}O_5$	4.37	-	2.45	10.45	1.25	-
Benzenes	Benzene,4-methoxy-2-methyl-1-(methylthio)-	$C_9H_{12}OS$	1.22	1.86	-	-	-	2.86
Esters	Diethyl Phthalate	$C_{12}H_{14}O_4$	-	-	7.20	-	5.04	-

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344 **Table 2.** Relative peak areas of main products from biomass torrefaction in Py-GC/MS.

Bio-oil fraction	Relative content (%)		
	200 °C	250 °C	300 °C
Phenols	-	-	9.58
2-Methoxy-4-vinylphenol	-	-	1.41
Syringol	-	-	0.55
Isoeugenol	-	-	1.92
2,6-Dimethoxy-4-allylphenol	-	-	5.70
Aldehydes	-	-	19.53
4-Methyl-2,5-dimethoxybenzaldehyde	-	-	2.41
3,5-Dimethoxy-4-hydroxybenzaldehyde	-	-	1.06
coniferyl aldehyde	-	-	8.37
3,5-Dimethoxy-4-hydroxycinnamaldehyde	-	-	7.69
Carbohydrates	-	-	3.07
1,6-Anhydro- β -D-glucopyranose(levoglucosan)	-	-	3.07
Esters	100	100	35.15
Diethyl Phthalate	100	100	35.15
Alcohols	-	-	2.09
Homovanillyl alcohol	-	-	0.44
2',4',6'-Trihydroxy-3'-methylbutyrophenone	-	-	1.65

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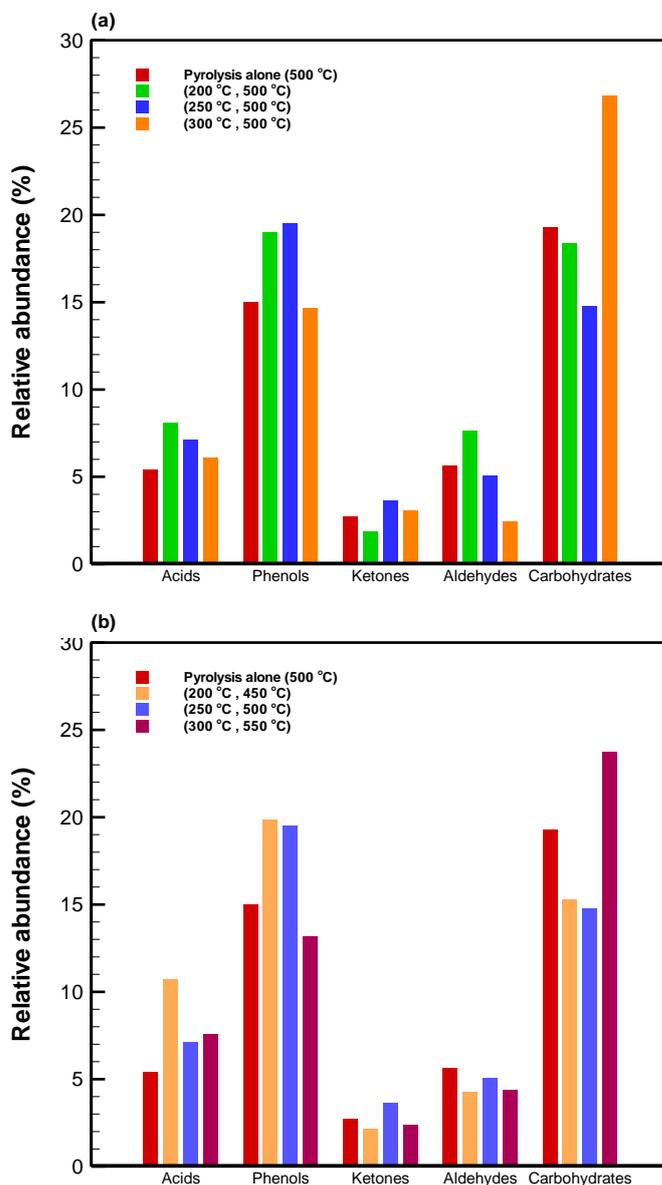
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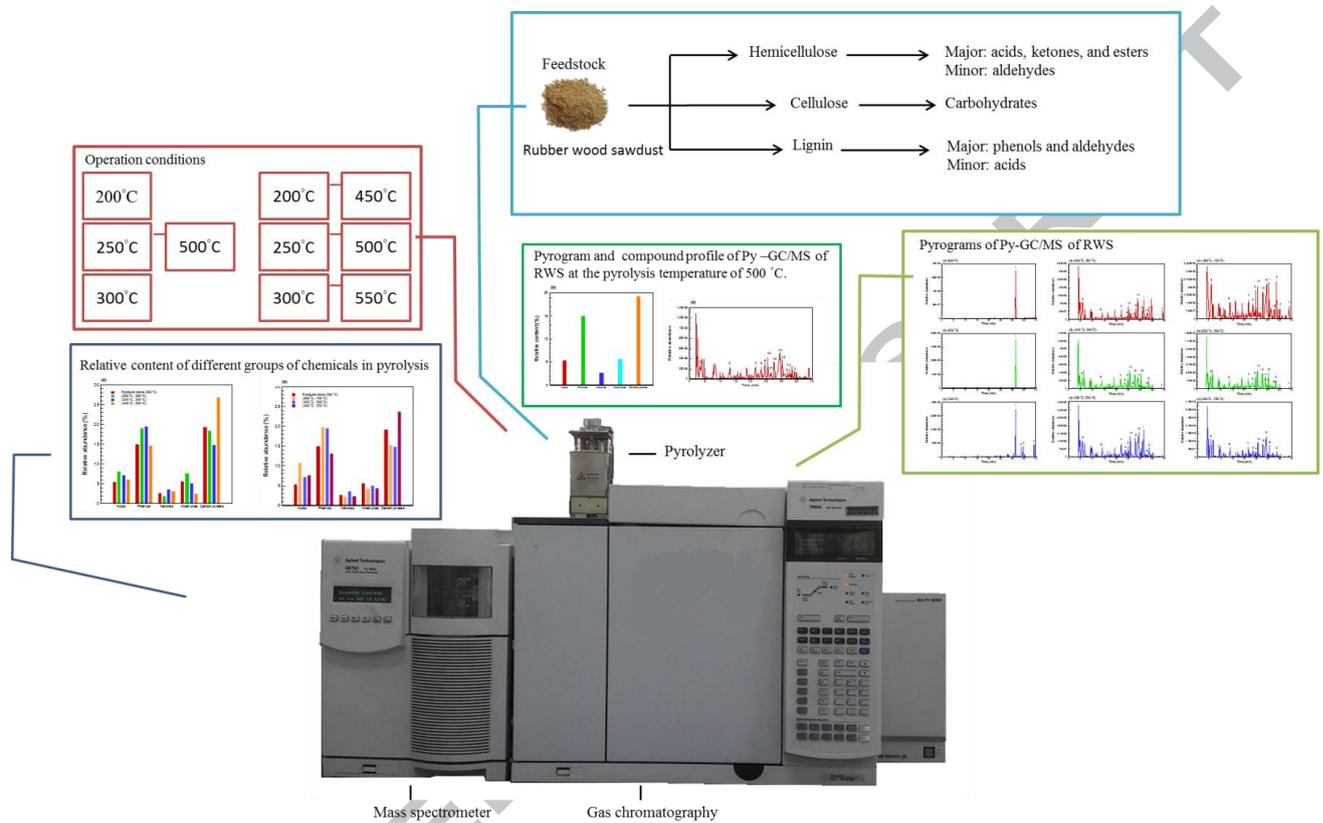
352 **Fig. 1.** Relative content profiles of five groups of compounds at the pyrolysis temperature
 353 of 500 °C along with the torrefaction temperatures of (a) 200 °C, (b) 250 °C, and (c)
 354 300 °C.

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Graphical abstract

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Highlights

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362 1. Effect of torrefaction on the pyrolysis of rubber wood sawdust is analyzed using
363 Py-GC/MS.

364 2. Hemicellulose degradation is exhibited at torrefaction temperatures of 200 and 250 °C.

365 3. Hemicellulose and lignin decomposition is predominant for the biomass torrefied at 300
366 °C.

367 4. Acids and aldehydes contents in pyrolysis bio-oil decrease with torrefaction temperature.

368 5. Relatively more cellulose is retained in the biomass when it is torrefied at 300 °C.

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